

Info

Jiří Kolafa

Department of Physical Chemistry

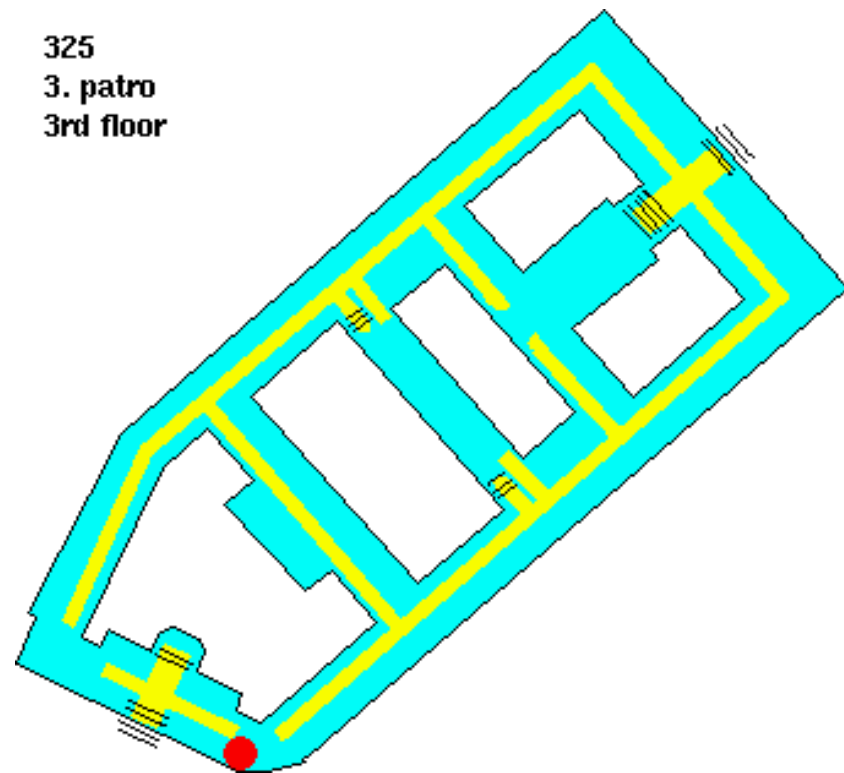
ICT Prague, building A, room 325

<http://www.mapy.cz/s/98vC>

jiri.kolafa@vscht.cz

220 444 257

Google: 🔍



- rate of reactions, dependence on conditions
- calculate the composition as a function of time
- reaction mechanisms



credit: people.bath.ac.uk/ch3mw/photo3.gif

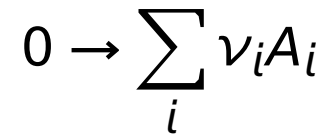
Chemical kinetics

Reactions:

- homogeneous (one phase)
- heterogeneous
- enzyme
- isothermal – adiabatic
- isobaric – isochoric

Activation:

- catalyst
- heat, other reaction, microwaves
- light (VIS, UV, X), ultrasound ...



reactants: $\nu_i < 0$
products: $\nu_i > 0$

Rate of reaction (ξ = extent of reaction, $[\xi] = \text{mol}$):

$$J = \frac{d\xi}{d\tau} = \frac{1}{\nu_i} \frac{dn_i}{d\tau}$$

Usually per unit volume (intensive quantity):

$$r = \frac{J}{V} = \frac{1}{\nu_i} \frac{dc_i}{d\tau}$$

● r depends on stoichiometry:

$$r(2A \rightarrow A_2) = \frac{1}{2} r(A \rightarrow \frac{1}{2} A_2)$$

concentration:

$$c_i = [A_i] = n_i/V$$

unit:

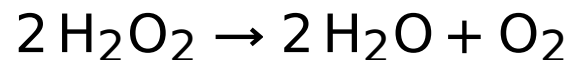
$$\text{mol dm}^{-3} = \text{mol/L} = \text{M}$$

dimensionless (relative)

concentration:

$$c_i^{\text{rel}} = \{A_i\} = c_i/c^{\text{st}}$$

Example. Hydrogen peroxide decomposes in the presence of a catalyst by rate $d[\text{H}_2\text{O}_2]/d\tau = -0.02 \text{ mol L}^{-1} \text{ min}^{-1}$. Determine the rate of the reaction



Simple reaction is given by one reaction and one kinetic equation (not necessarily elementary)

Generally:

$$r = f(c_A, c_B, \dots, T)$$

Often:

$$r = k(T) c_A^\alpha c_B^\beta \dots$$

where

- $k(T)$ = rate constant (kinetic constant)
- α, β = partial orders of reaction (elem.r. = integers)
- $n = \alpha + \beta \dots$ = (total) reaction order

Dimensionality(k) = $(\text{mol dm}^{-3})^{1-n} \text{s}^{-1}$

Often dimensionless $c_i^{\text{rel}} = c_i/c^{\text{st}}$, then dimension(k) = s^{-1}

Half life of reaction: c_A decreases to one half

$$c_A(\tau_{1/2}) = \frac{c_A(0)}{2}$$

$$0 \rightarrow \sum_i \nu_i A_i$$

Constant volume: balance in concentrations ($x = x(\tau) = \xi/V$):

$$c_i = c_{i,0} + \nu_i x$$

Degree of conversion ($k = \text{key compound} \Rightarrow \nu_k < 0$):

$$\alpha = \frac{c_{k,0} - c_k}{c_{k,0}} = \frac{|\nu_k| x}{c_{k,0}}$$

It holds $0 \leq \alpha \leq 1$

Example. Nitryl fluoride is produced in gas phase by reaction:



The reaction is of the 1st order with respect to both NO_2 and F_2 . Write the kinetic equation if the reaction proceeds in constant volume. The initial concentrations are $[\text{NO}_2]_0$ and $[\text{F}_2]_0$, respectively, and the kinetic constant k .

$$\frac{dx}{d\tau} = -\frac{d[\text{F}_2]}{d\tau} = -\frac{1}{2} \frac{d[\text{NO}_2]}{d\tau} = \frac{1}{2} \frac{d[\text{NO}_2\text{F}]}{d\tau} = k([\text{NO}_2]_0 - 2x)([\text{F}_2]_0 - x)$$

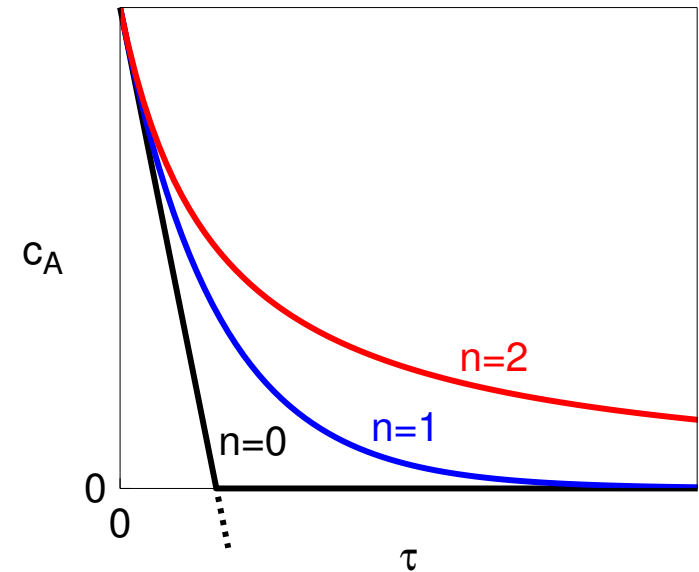
Reaction A → P

Rate equation:

$$\begin{aligned} \frac{dc_A}{d\tau} &= -kc_A^n \quad \text{for } c_A > 0 \\ &= 0 \quad \text{for } c_A = 0 \end{aligned}$$

Initial condition: $c_A(0) = c_{A0}$

Solution (integrated form):



n	$c_A(\tau)$	conditions	$\tau_{1/2}$
0	$c_{A0} - k\tau$ 0	$\tau < c_{A0}/k$ $\tau \geq c_{A0}/k$	$\frac{c_{A0}}{2k}$
1	$c_{A0} e^{-k\tau}$		$\ln 2/k$
2	$\frac{1}{1/c_{A0} + k\tau}$		$\frac{1}{kc_{A0}}$
$(1, \infty)$	$[c_{A0}^{1-n} - (1-n)k\tau]^{1/(1-n)}$		
$[0, 1)$	$[c_{A0}^{1-n} - (1-n)k\tau]^{1/(1-n)}$ 0	$\tau < c_{A0}^{1-n}/[(1-n)k]$ $\tau \geq c_{A0}^{1-n}/[(1-n)k]$	$\frac{2^{n-1}-1}{(n-1)k} c_{A0}^{1-n}$

Reaction $A + B \rightarrow P$ (1st order to both A and B)

Both partial orders $\alpha = \beta = 1$ (total order = 2)

Rate equation:

$$\frac{dx}{d\tau} = kC_A C_B = k(C_{A0} - x)(C_{B0} - x)$$

Initial condition:

$$x(0) = 0 \text{ or } C_A(0) = C_{A0}, C_B(0) = C_{B0},$$

Solution (integrated form):

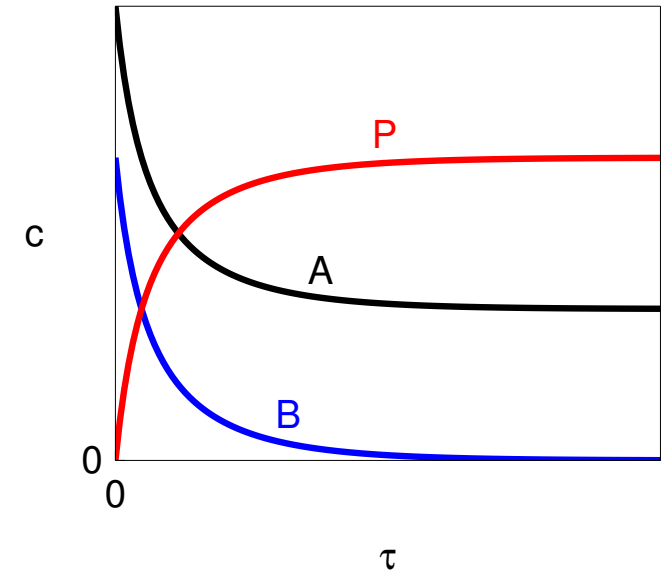
● $C_{A0} = C_{B0}$: the same as previous slide

● $C_{A0} \neq C_{B0}$: $(C_{A0} - C_{B0})k\tau = \ln\left(\frac{C_{A0} - x}{C_{B0} - x} \frac{C_{B0}}{C_{A0}}\right) = \ln\left(\frac{C_A}{C_B} \frac{C_{B0}}{C_{A0}}\right) \Rightarrow$

$$C_A = (C_{A0} - C_{B0}) \frac{C_{A0} \epsilon}{C_{A0} \epsilon - C_{B0}}$$

$$C_B = (C_{A0} - C_{B0}) \frac{C_{B0}}{C_{A0} \epsilon - C_{B0}} \text{ where } \epsilon = \exp[(C_{A0} - C_{B0})k\tau]$$

$$\exp x = e^x$$



Example: $\text{NO}_2^-(\text{aq}) + \text{NH}_4^+(\text{aq}) \rightarrow \text{N}_2(\text{g}) + 2 \text{H}_2\text{O}(\text{l})$

- Integral data: $c_i(\tau)$
- Differential data: rates $dc_i/d\tau$:
 - flow reactor (steady state) $dc_i/d\tau \propto c_i^{\text{in}} - c_i^{\text{out}}$
 - initial reaction rate (small extent)

symbol \propto means
“proportional to”

- Fast reaction: lasers

Proxies to $c_i(\tau)$:

- mechanical:
 - (g): pressure (manometry) / volume (volumetry)
 - (l): difference of volume (dilatometry), densitometry
 - (s/g): mass (gravimetry)
 - (l/g): vapor pressure
- optical: spectrophotometry, refractometry, polarimetry
- electric: conductometry, potentiometry, polarography
- chromatography, mass spectrometry

Determining the order and rate constant

Example. For reaction $A \rightarrow P$ with rate equation $dc/dt = -kc^n$

● **Fitting** (correlation, regression):

the integrated form of the kinetic equation, $c_A = c_A(c_{A0}, k, n; \tau)$, is fitted to the data by the **least square method**

The sum of squares is minimized over **3** unknowns parameters c_{A0}, k, n

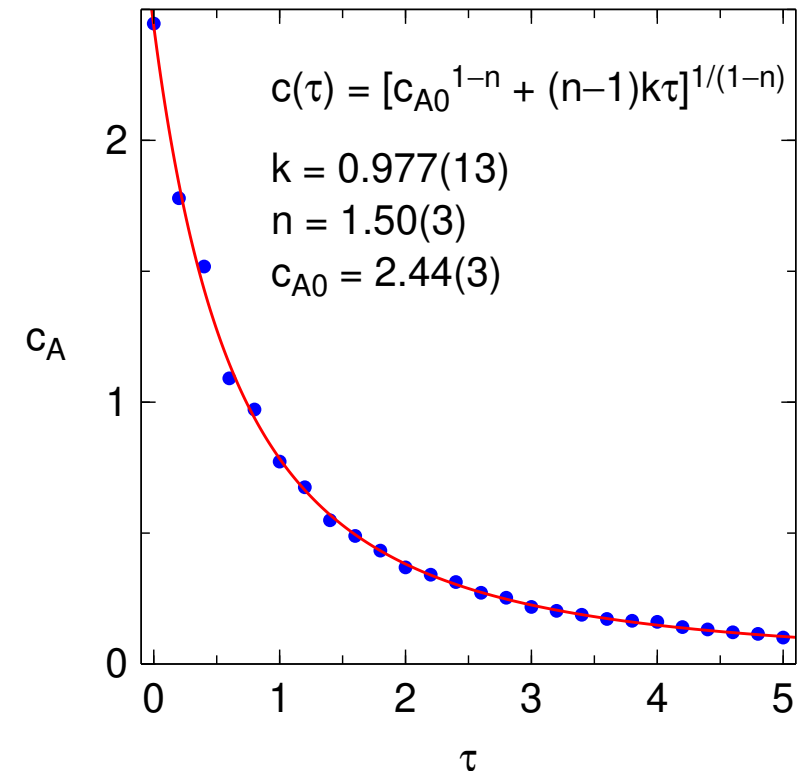
τ min	c mol L ⁻¹	τ min	c mol L ⁻¹	τ min	c mol L ⁻¹	τ min	c mol L ⁻¹
0.0	2.446	1.4	0.549	2.8	0.253	4.2	0.141
0.2	1.779	1.6	0.489	3.0	0.218	4.4	0.132
0.4	1.518	1.8	0.433	3.2	0.203	4.6	0.121
0.6	1.091	2.0	0.369	3.4	0.188	4.8	0.115
0.8	0.972	2.2	0.341	3.6	0.172	5.0	0.101
1.0	0.773	2.4	0.313	3.8	0.165		
1.2	0.675	2.6	0.272	4.0	0.161		

Mathematically:

$$s^2 = \min_{c_{A0}, k, n} \frac{1}{N-3} \sum_{i=1}^N \left[\frac{c_A(c_{A0}, k, n; \tau) - c_i}{\sigma_i} \right]^2$$

where σ_i = standard error^a of conc. $c_{A,i}$ (its estimate); for large N then $s^2 = 1$. If σ_i are not known, they can be calculated from $s^2 = 1$ assuming that all σ_i are the same.

^aor uncertainty – called differently in statistics and in metrology



- **Integral method** trial-and-error: For several orders n , we calculate the rate constant from pairs $c(\tau_1), c(\tau_2)$.

For $A \rightarrow P$:

$$k = \begin{cases} \frac{c_{A1}^{1-n} - c_{A2}^{1-n}}{(n-1)(\tau_1 - \tau_2)} & n \neq 1 \\ \frac{\ln(c_{A1}/c_{A2})}{\tau_1 - \tau_2} & n = 1 \end{cases}$$

Example (see previous data):

τ_1	τ_2	$n = 1$	$n = 2$	$n = 1.5$
0	1	1.152	0.885	0.996
1	2	0.739	1.416	1.018
2	3	0.526	1.877	0.991
3	4	0.303	1.624	0.701
4	5	0.466	3.690	1.309

- **Differential method**: rates for two times (or compositions) known

$$n = \frac{\ln(r_1/r_2)}{\ln(c_{A1}/c_{A2})}$$

- **Isolation method** (Ostwald):

$$r = kc_A^\alpha c_B^\beta : c_B \gg c_A \text{ (surplus B)} \Rightarrow r = k'c_A^\alpha$$

Now obsolete!

● integral method

1. order: $\ln c_A = \ln c_{A0} - k\tau \Rightarrow$ straight line in $(\tau, \ln c_A)$

2. order: $-1/c_A = -1/c_{A0} - k\tau \Rightarrow$ straight line in $(\tau, -1/c_A)$

$\frac{3}{2}$. order: $-2/c_A^{1/2} = -2/c_{A0}^{1/2} - k\tau \Rightarrow$ straight line in $(\tau, -2/c_A^{1/2})$

● differential method

- tangent to $c_A(\tau) \Rightarrow$ derivative $r(\tau)$

- $\ln r = \ln k + n \ln c_A \Rightarrow$ straight line in $(\ln c_A, \ln r)$

Consecutive reactions of the 1st order



Kinetic equations:

$$\frac{dc_A}{d\tau} = -k_1 c_A$$

$$\frac{dc_B}{d\tau} = k_1 c_A - k_2 c_B$$

$$\frac{dc_C}{d\tau} = k_2 c_B$$

Initial conditions:

$$c_A(0) = c_{A0}, \quad c_B(0) = 0, \quad c_C(0) = 0$$

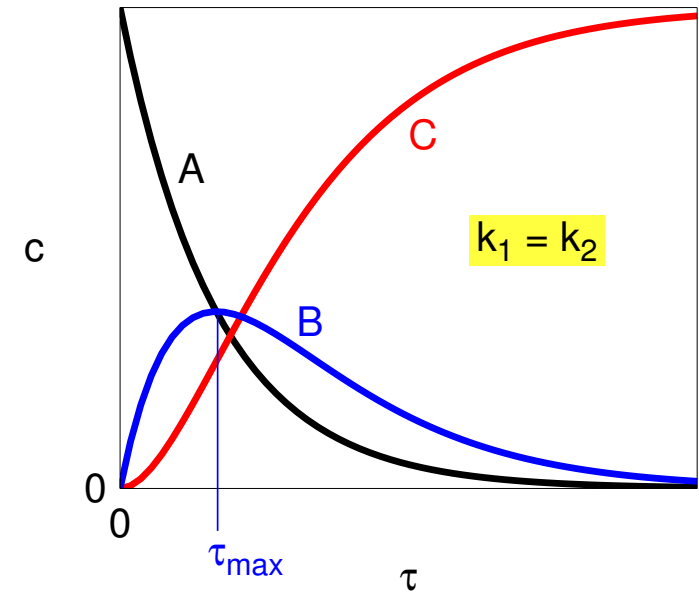
Solution:

$$c_A = c_{A0} e^{-k_1 \tau}$$

$$c_B = \frac{k_1}{k_2 - k_1} c_{A0} \left[e^{-k_1 \tau} - e^{-k_2 \tau} \right] \quad \text{for } k_1 \neq k_2$$

$$= k_1 c_{A0} \tau e^{-k_1 \tau} \quad \text{for } k_1 = k_2$$

$$c_C = c_{A0} - c_A - c_B$$



Max. concentration:

$$\tau_{\max} =$$

$$\frac{\ln(k_1/k_2)}{k_1 - k_2} \quad \text{for } k_1 \neq k_2$$

$$1/k_1 \quad \text{for } k_1 = k_2$$

- radioactive decay
- pharmacokinetics:
 - k_1 = absorption const.
 - k_2 = elimination const.

Distribution volume V_d is the volume of water in which the dissolved drug would have the same concentration as it has in blood plasma.

$$V_d = \frac{\text{mass of drug}}{\text{mass conc. in plasma}}$$

Often give per 1 kg of patient's weight

$$V_d = \frac{\text{mass of drug}}{(\text{mass conc. in plasma}) \times (\text{mass of patient})}$$

volume	$V_d / (\text{L kg}^{-1})$	
water total	0.6	children more, seniors less
intracellular	0.4	
extracellular	0.2	
blood total	0.08	
plasma	0.04–0.05	

- water-soluble compound, permeates through membranes, does not bind to anything: $V_d \approx 0.6 \text{ L kg}^{-1}$ (e.g., ethanol)
- lipophilic compound: higher (even hundreds)
- slow permeation through membranes etc.: more compartments needed

Application to pharmacokinetics

Simplification:

- one compartment
- 1st order kinetics (other options: 0th order, Michaelis–Menten)
- absorption k_1 , elimination k_2
- “initial” weight concentration:

$$C_{A0} = \frac{\text{mass of drug}}{\text{mass of patient} \times V_d}$$

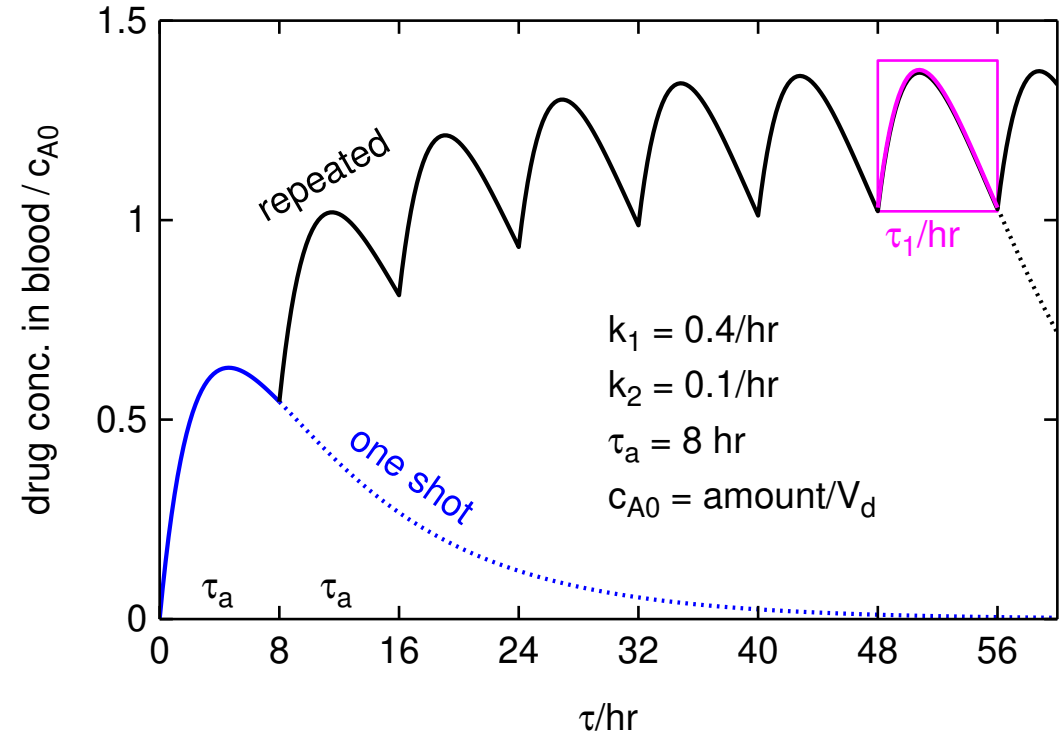
One shot

see “consecutive reactions”

Repeated shots

k -times by τ_a

(in times $0, \tau_a, 2\tau_a, \dots, (k-1)\tau_a$)



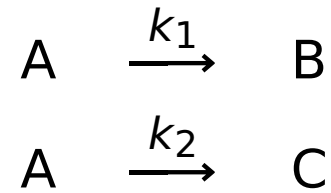
After many cycles (∞ series) for $\tau_1 = \tau - (k-1)\tau_a =$ time from the last shot:

$$C_B = \frac{k_1 C_{A0}}{k_2 - k_1} \left[\frac{e^{-k_1 \tau_1}}{1 - e^{-k_1 \tau_a}} - \frac{e^{-k_2 \tau_1}}{1 - e^{-k_2 \tau_a}} \right], k_1 \neq k_2$$

$$= \frac{k_1 C_{A0} e^{-k_1 \tau_1}}{1 - e^{-k_1 \tau_a}} \left[\tau + \frac{\tau_a e^{-k_1 \tau_a}}{1 - e^{-k_1 \tau_a}} \right], k_1 = k_2$$

Concurrent reactions

Example. Both reactions of the first order



Rate equations:

$$\frac{dc_A}{d\tau} = -k_1 c_A - k_2 c_A$$

$$\frac{dc_B}{d\tau} = k_1 c_A$$

$$\frac{dc_C}{d\tau} = k_2 c_A$$

Solution for $c_A(0) = c_{A0}$, $c_B(0) = 0$, $c_C(0) = 0$:

$$c_A = c_{A0} \exp[-(k_1 + k_2)\tau]$$

$$c_B = c_{A0} \frac{k_1}{k_1 + k_2} \{1 - \exp[-(k_1 + k_2)\tau]\}$$

$$c_C = c_{A0} \frac{k_2}{k_1 + k_2} \{1 - \exp[-(k_1 + k_2)\tau]\}$$

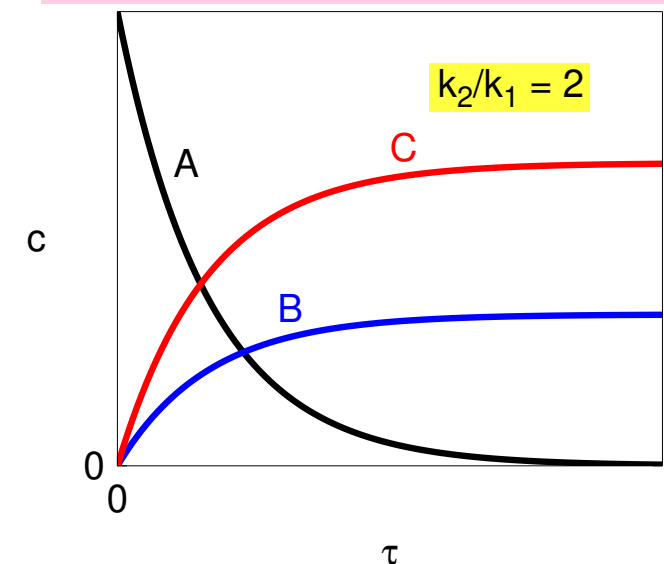
Variants: $A+B \rightarrow$, $A+C \rightarrow$, $A \gg B, C$



Rudolf Wegscheider
credit: Wikipedia

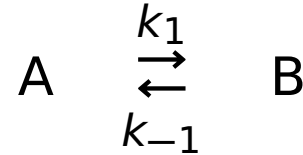
if both reactions are of the same order:
Wegscheider principle:

$$\frac{c_B}{c_C} = \frac{k_1}{k_2}$$



Reversible reactions

Example. Both reactions of the 1st order:



Rate equation:

$$\frac{dc_A}{d\tau} = -k_1 c_A + k_{-1} c_B$$

Balance for $c_A(0) = c_{A0}$, $c_B(0) = 0$:

$$c_A + c_B = c_{A0}$$

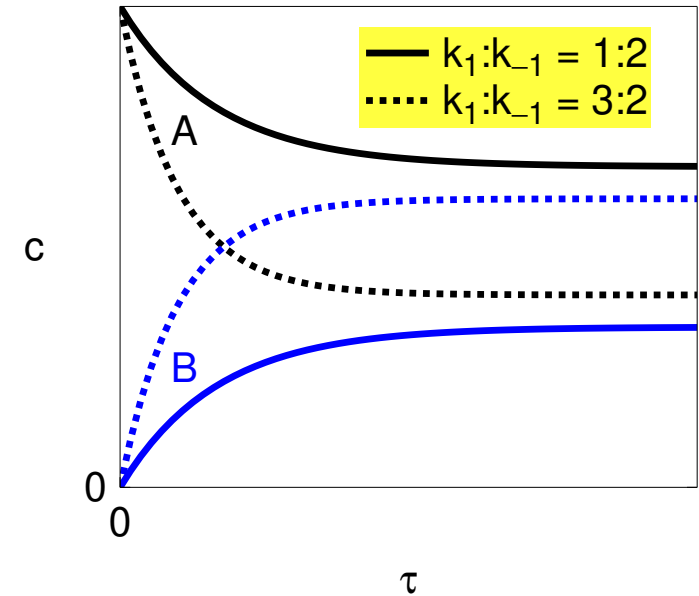
Solution:

$$c_A = \frac{c_{A0}}{k_1 + k_{-1}} \left[k_1 e^{-(k_1 + k_{-1})\tau} + k_{-1} \right]$$

Equilibrium:

$$\lim_{\tau \rightarrow \infty} c_A = \frac{k_{-1}}{k_1 + k_{-1}} c_{A0}$$

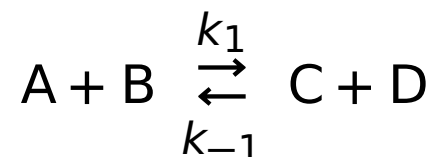
Equilibrium constant: $\frac{c_B(\infty)}{c_A(\infty)} = \frac{k_1}{k_{-1}} = K$



racemization (1 chiral C): $K = 1$

Guldberg-Waage:

Let both reactions in



are elementary (of 1st order wrt all compounds)

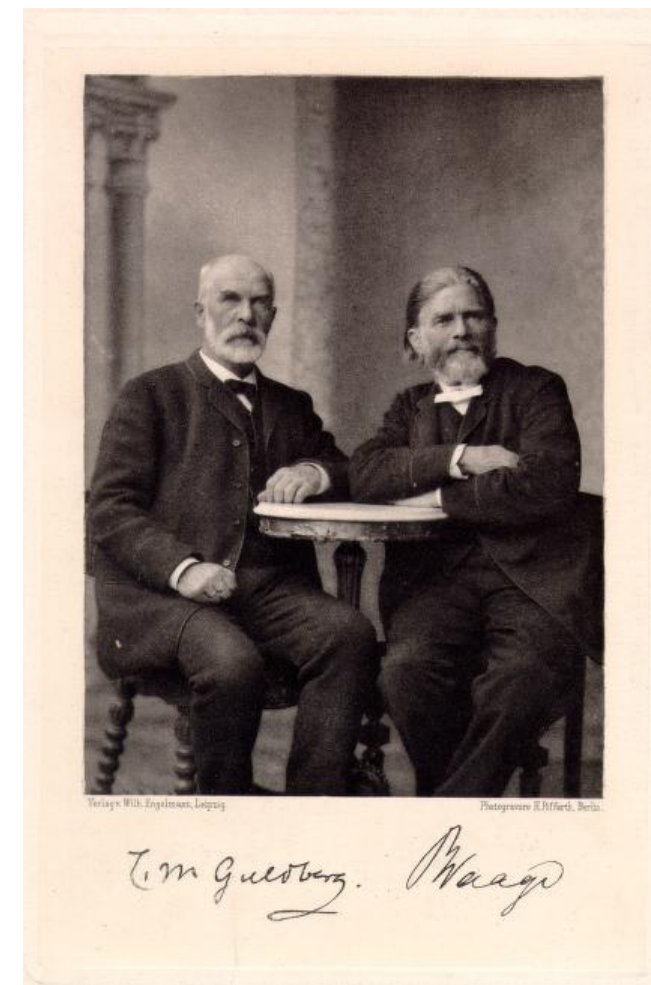
Rate equation:

$$\frac{dc_A}{d\tau} = -k_1 c_A c_B + k_{-1} c_C c_D$$

Equilibrium: $\frac{dc_A}{d\tau} = 0$ or

$$\frac{c_C c_D}{c_A c_B} = \frac{k_1}{k_{-1}} = K$$

where K is the equilibrium constant



credit: Wikipedia

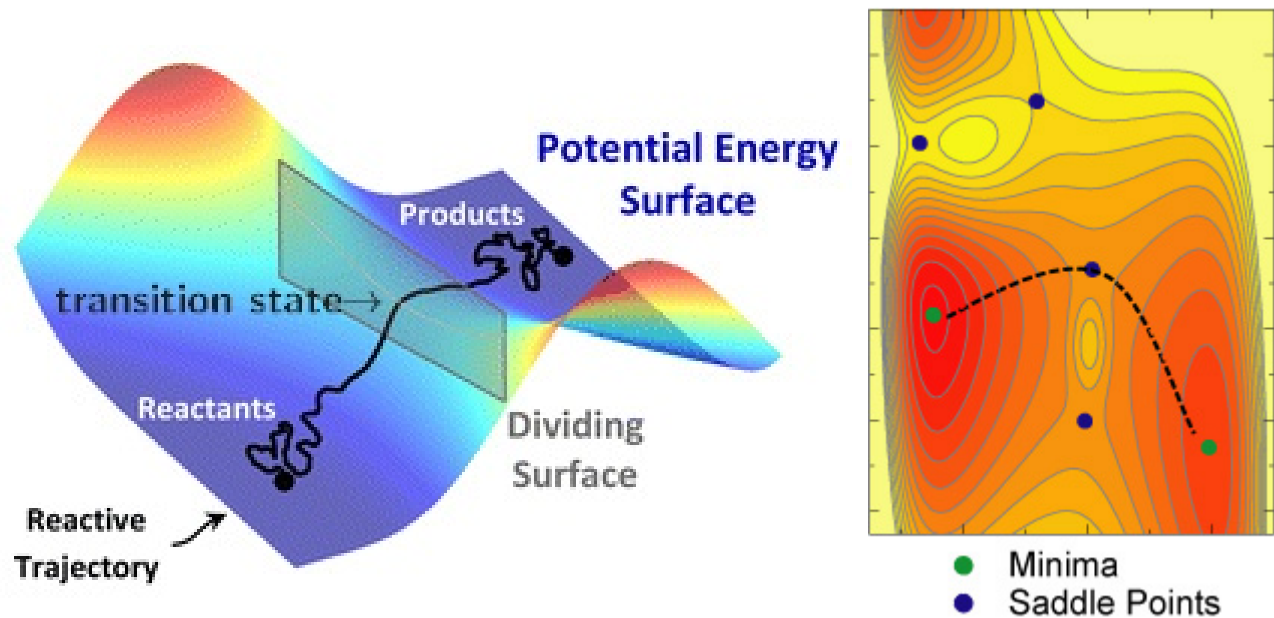
Potential energy surface (PES)

Nuclei are much heavier than electrons \Rightarrow electrons are faster (Born–Oppenheimer approximation): electrons follow nuclei

Potential energy surface: energy as a function of coordinates of all nuclei

Better: after removing redundant coordinates because of symmetry (rotations, translations)

A reaction proceeds by the least obstacle way = over the saddle point (better: close to it) = **transition state**

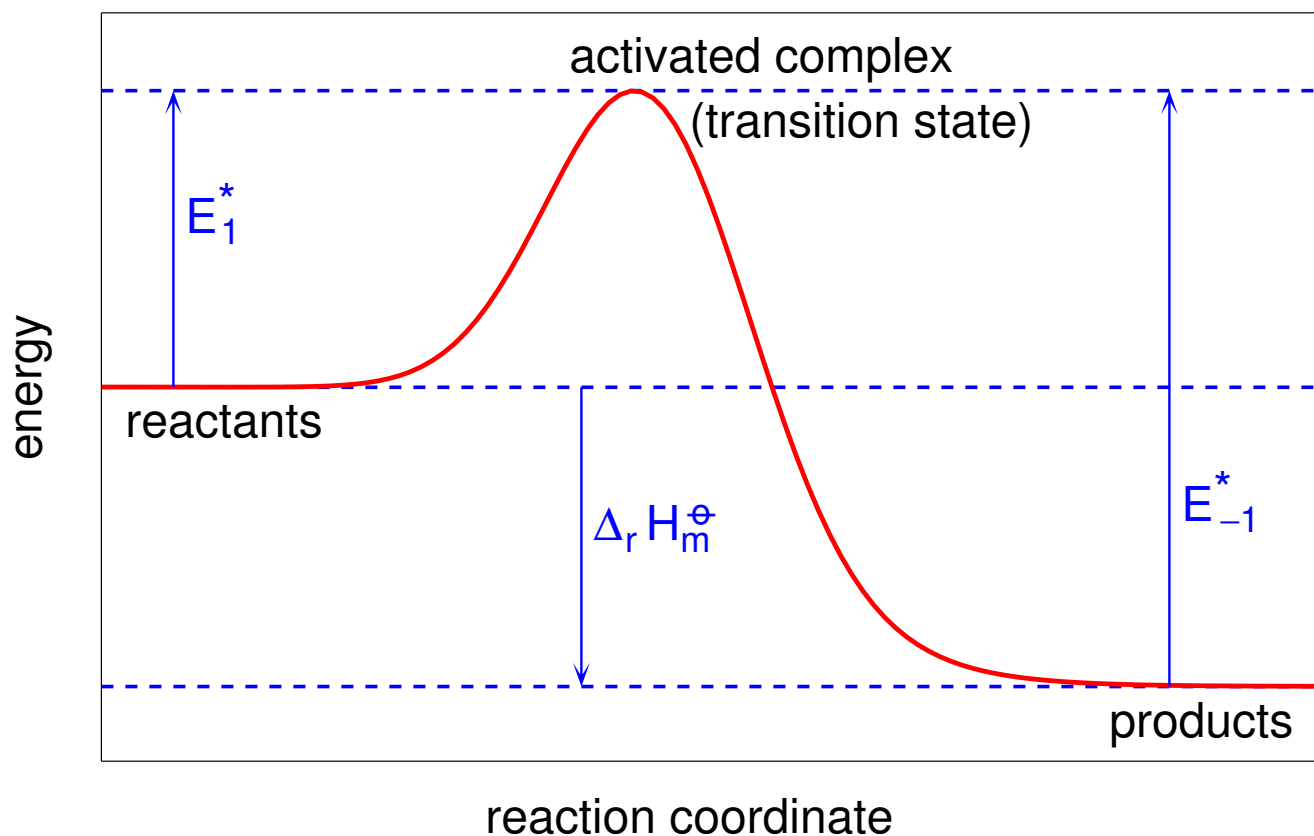


credits: <http://www.ucl.ac.uk/~ucecmst/publications.html>, <http://theory.cm.utexas.edu/henkelman/research/ltd/>

Transition state theory (Eyring): $k = (RT/N_A h) \exp(-[G_m^\ddagger - G_m^{\text{reactants}}]/RT)$

$$\frac{d \ln K}{dT} = \frac{\Delta_r H_m^\ominus}{RT^2} \quad \Delta_r H_m^\ominus = \text{const} \Rightarrow K = K_0 e^{-\frac{\Delta_r H_m^\ominus}{RT}} = \frac{k_1}{k_{-1}} = \frac{A_1 e^{-\frac{E_1^*}{RT}}}{A_2 e^{-\frac{E_{-1}^*}{RT}}} \Rightarrow k = A e^{-\frac{E^*}{RT}}$$

E^* = **activation energy**, A = prefactor



$$\Delta_r H_m^\ominus = E_1^* - E_{-1}^*$$

Typical E^* :
50–110 kJ mol⁻¹

Rule of the thumb:
1.5–3× per 10 °C

Kinetic theory of gases (Boltzmann): $k = 2N_A \sigma (RT/\pi M)^{1/2} \exp(-E^*/RT)$