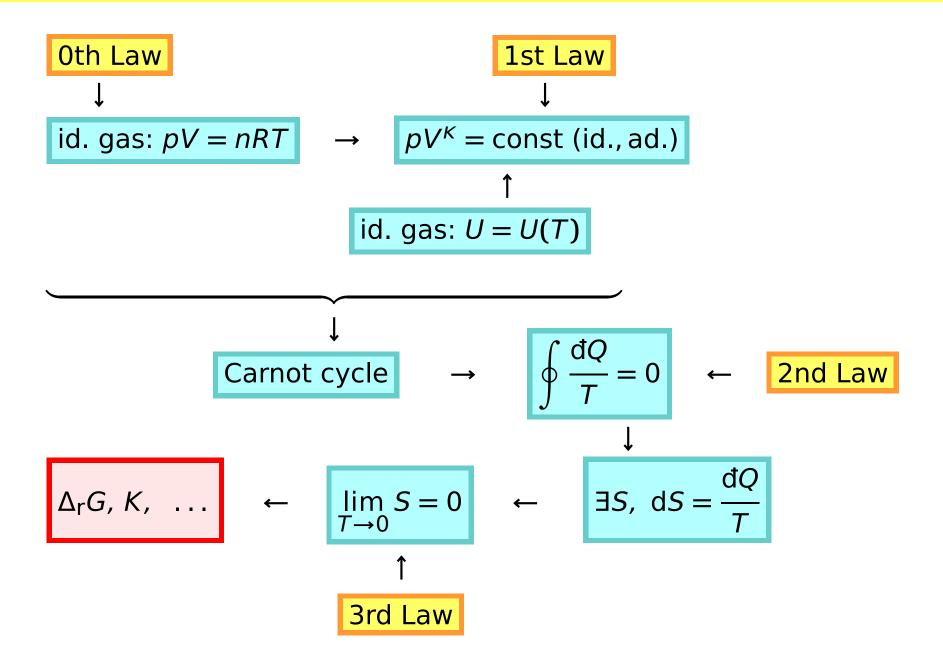
Overview of classical thermodynamics



More about entropy

[pic/entropy.sh] 2/16 *col*03

Consider a **reversible** adiabatic process (dQ = 0)

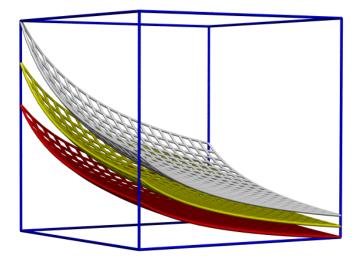
In well-chosen variables (e.g., T, V, p) the system moves on a (hyper)surface

- Heat: surface † surface Cool: surface ↓ surface
- Energy dissipation (**irreversible** process: work \rightarrow energy) \Rightarrow surface \uparrow surface
- Surfaces have constant entropy

Entropy increases **↑** in the dirrection of adding heat/energy dissipation

Carathédory: In every neighborhood of any state *S* of an adiabatically enclosed system there are states inaccessible from *S*.

 \Rightarrow 3 function of empirical temperature so that f dQ is a total differential; then $1/f \propto T$





credit: Wikipedia

Helmholtz and Gibbs energies

Internal energy

↓Gibbs eq.↓

$$U(S, V) dU = T dS - p dV$$

Enthalpy

$$H(S, p) = U + pV = U - \left(\frac{\partial U}{\partial V}\right)V \Rightarrow dH = TdS + Vdp$$

Helmholtz (free) energy (Helmholtz function, free (internal) energy)

$$F(T, V) = U - TS = U - \left(\frac{\partial U}{\partial S}\right)S \Rightarrow dF = -SdT - pdV$$

Often denoted by A

Gibbs (free) energy (Gibbs function, free enthalpy)

$$G(T, p) = H - TS = H - \left(\frac{\partial H}{\partial S}\right)S \Rightarrow dG = -SdT + Vdp$$

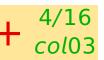
Or: $G = F + pV = F - \left(\frac{\partial F}{\partial V}\right)V$

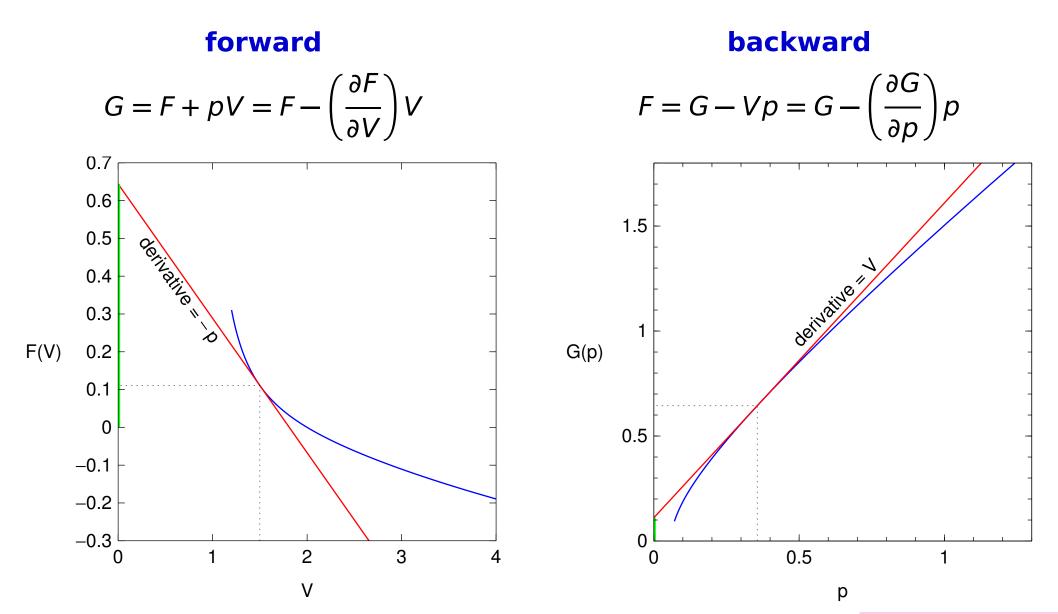
avoid term "free energy" unless it is clear whether it is Gibbs or Helmholtz

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Mathematical context (Legendre transform)





The transf. is well-defined (gives one value) if F(V) is convex. Then G(p) is concave and there exists a back-transform.

The curves are calculated from the van der Waals equation

Calculation of *G*

= H - TS

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Example—one phase transition.

$$H(T_{2}, p) = H(T_{1}, p) + \int_{T_{1}}^{T_{fp}} C_{p} dT + \Delta_{fp} H + \int_{T_{fp}}^{T_{2}} C_{p} dT$$
$$S(T_{2}, p) = S(T_{1}, p) + \int_{T_{1}}^{T_{fp}} \frac{C_{p}}{T} dT + \frac{\Delta_{fp} H}{T_{fp}} + \int_{T_{fp}}^{T_{2}} \frac{C_{p}}{T} dT$$
$$low T : \quad S(T_{1}, p) = \int_{0}^{\approx 15 \text{ K}} \frac{\text{const} T^{3}}{T} dT + \cdots$$
$$H(T, p_{2}) = H(T, p_{1}) + \int_{p_{1}}^{p_{2}} \left[V - T \left(\frac{\partial V}{\partial T} \right)_{p} \right] dp$$
$$S(T, p_{1}) = S(T, p_{2}) - \int_{p_{1}}^{p_{2}} \left(\frac{\partial V}{\partial T} \right)_{p} dp$$

We can predict chemical equilibria from thermochemistry and EoS data!

F, G and work—reversible processes

 $\mathrm{d}U = T\mathrm{d}S + \mathrm{d}W$

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$$dF = -SdT + dW \implies dF = dW [T]$$

Change of the Helmholtz energy at const. T = work

 $dW = -p dV + dW_{other than pressure-volume}$

 $dG = -SdT + Vdp + dW_{other than pressure-volume}$

= $dW_{other than pressure-volume}$ [*T*, *p*]

Change of the Gibbs energy at const. T, p= work other than pressure-volume

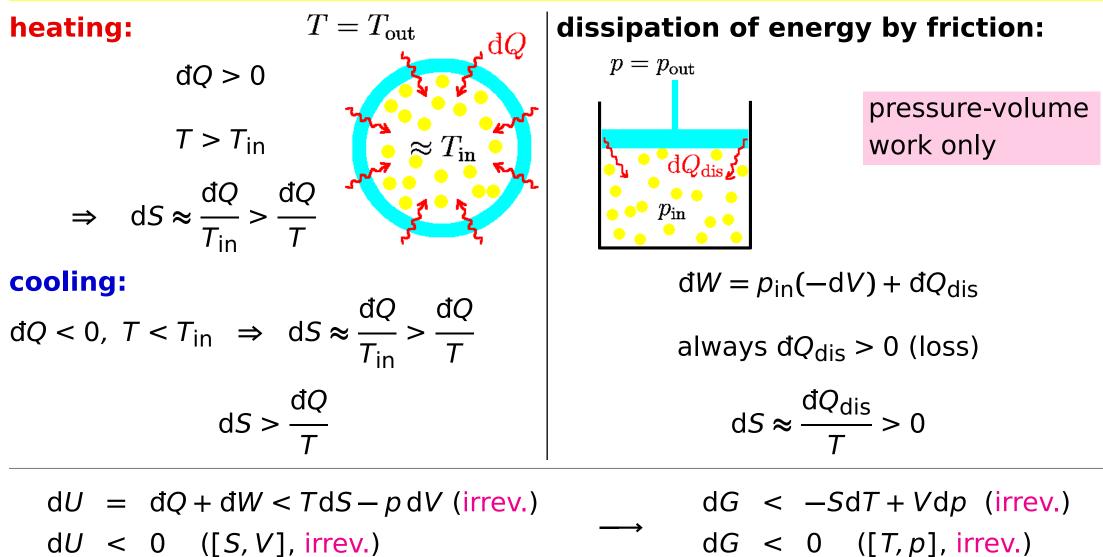
Interpretation of terms F = U - TS (G = H - TS)

Iow temperature \Rightarrow the influence of **energy** (enthalpy) > of entropy

high temperature \Rightarrow the influence of **entropy** > energy (enthalpy)

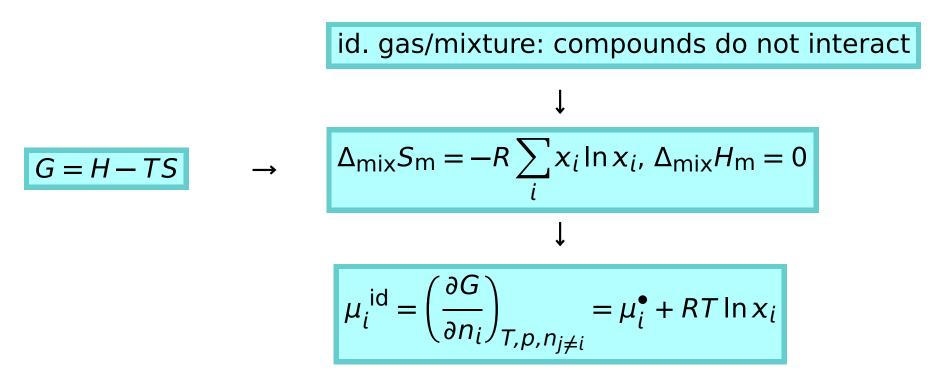
Irreversible processes

dU < 0 ([*S*, *V*], irrev.)



The Gibbs energy of a closed system at constant T, p spontaneously (via irreversible processes) decreases. In equilibrium it reaches a minimum.

Chemical potential



Chemical potential μ_i of compound *i* (w.r.t a standard state) = reversible work needed to transform 1 mole of the compound (from the standard state) to the given state = "ability to perform this work"

Example. How much energy is needed to obtain 1 m^3 of fresh water from sea water (3.5 wt.% NaCl, 300 K)?

Activity and the chemical potential

General definition:

$$u_i = \mu_i^{\oplus} + RT \ln a_i$$

 \Rightarrow = plimsoll

for substance *i* in a standard state it holds $a_i = 1$

Standard state overview:

$$a_{i}^{\circ} = \frac{p_{i}}{p^{\text{st}}} \gamma^{\circ} = \frac{x_{i}p}{p^{\text{st}}} \gamma^{\circ} \quad p_{i} \to 0$$

$$a_{i}^{\bullet} = x_{i}\gamma_{i}^{\bullet} \quad x_{i} \to 1$$

$$a_{i}^{[x]} = x_{i}\gamma_{i}^{[x]} \quad x_{i} \to 0$$

$$a_{i}^{[c]} = \frac{c_{i}}{c^{\text{st}}} \gamma_{i}^{[c]} \quad c_{i} \to 0$$

$$a_{i}^{[m]} = \frac{m_{i}}{m^{\text{st}}} \gamma_{i}^{[m]} \quad \underline{m}_{i} \to 0$$

In the respective limit $\gamma^{\circ} = 1$

 γ° is called a fugacity coefficient, usu. denoted φ or ν

Chemical equilibrium—balance

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General reaction:

$$0 = \sum_{i=1}^{k} v_i R_i \quad v_i < 0 \text{ (reactants), } v_i > 0 \text{ (products)}$$



ξ = **extent of reaction**; units [ξ] = mol

Let 1=key compound = first to be consumed $(n_1 = 0) \Rightarrow \xi = \xi_{max}$. Degree of reaction:

$$\alpha = \frac{n_{1,0} - n_1}{n_{1,0}} = -\frac{\nu_1 \xi}{n_{1,0}} = \frac{\xi}{\xi_{\text{max}}}$$

Equilibrium and *G*

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At [*T*, *p*] we look for the minimum of

$$G(n_1,\ldots,n_k)=\sum_{i=1}^k n_i\mu_i$$

where

$$n_1 = n_{1,0} + \nu_1 \xi, \dots, n_k = n_{k,0} + \nu_k \xi$$

in interval $\xi \in [\xi_{min}, \xi_{max}]$ (in homogeneous systems: in $\xi \in (\xi_{min}, \xi_{max})$) NB: $\mu_i = \mu_i(n_1, \dots, n_k)$

Minimum condition:

$$\left(\frac{\partial G}{\partial \xi}\right)_{p,T} = \sum_{i=1}^{k} \nu_{i} \mu_{i} \equiv \Delta_{r} G_{m} = 0$$

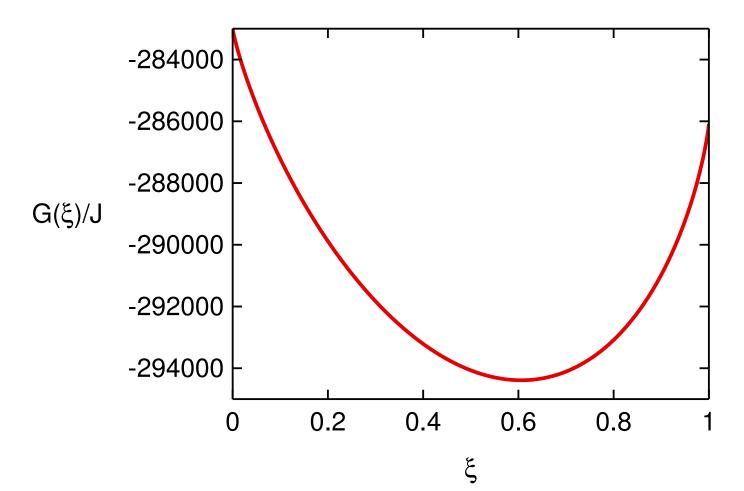
 $\Delta_r G_m$ = reaction Gibbs energy

	direction	name of
$\Delta_{\rm r}G_{\rm m}$	of reaction	reaction
< 0		exergonic
= 0	equilibrium	isoergonic
> 0	~~~~	endergonic

Exergy (availability, available energy) = maximum work a system may deliver upon transition to equilibrium

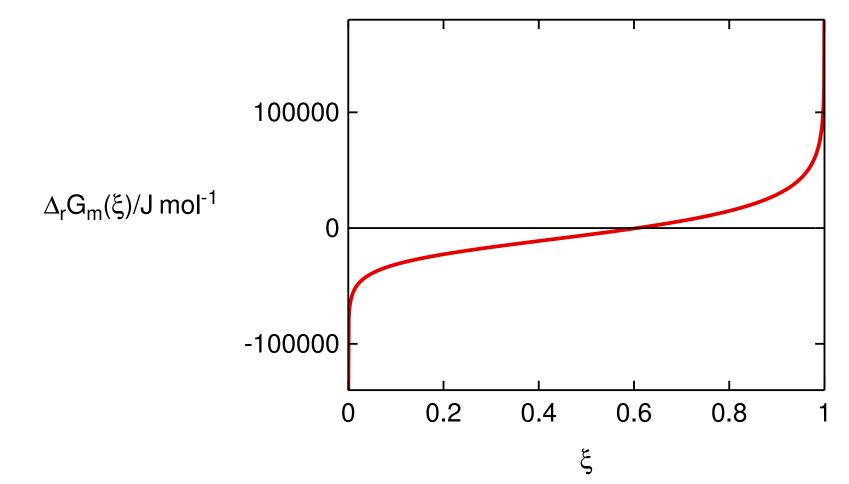
 $N_2 + 3H_2 \rightarrow 2NH_3$ (600 K, 10.13 MPa)

Initial composition: $n_{N_2,0} = 1 \text{ mol}$, $n_{H_2,0} = 3 \text{ mol}$, $n_{NH_3,0} = 0 \text{ mol}$ $G(\xi) = n_{NH_3}\mu_{NH_3} + n_{H_2}\mu_{H_2} + n_{N_2}\mu_{N_2} = 2\xi\mu_{NH_3} + (3 - 3\xi)\mu_{H_2} + (1 - \xi)\mu_{N_2}$



 $N_2 + 3H_2 \rightarrow 2NH_3$ (600 K, 10.13 MPa)

Initial composition: $n_{N_2,0} = 1 \text{ mol}$, $n_{H_2,0} = 3 \text{ mol}$, $n_{NH_3,0} = 0 \text{ mol}$ $\Delta_r G_m(\xi) = \nu_{NH_3} \mu_{NH_3} + \nu_{H_2} \mu_{H_2} + \nu_{N_2} \mu_{N_2} = 2\mu_{NH_3} - 3\mu_{H_2} - \mu_{N_2}$



Equilibrium constant

$$\mu_{i} = \mu_{i}^{\oplus} + RT \ln a_{i}$$
$$\Delta_{r}G_{m} = \Delta_{r}G_{m}^{\oplus} + RT \ln \prod_{i=1}^{k} a_{i}^{\nu_{i}} \quad \text{in equilibrium} \quad 0$$

Definition of the equilibrium constant*:

$$K = \exp\left(-\frac{\Delta_{\rm r} G_{\rm m}^{\oplus}}{RT}\right)$$

 \Rightarrow equilibrium condition:

$$K = \prod_{i=1}^{k} a_i^{\nu_i} \qquad \left(\frac{\text{products}}{\text{reactants}}\right)$$

Given Set in S

smaller K: more reactants (\leftarrow)

*According to IUPAC gold book, this *K* is "standard" or "thermodynamic" equilibrium constant. Just "equilibrium constant" may be based on concentrations, fugacities, or molalities and may have dimension.

Direction of a reaction

$$\Delta_{\rm r}G_{\rm m} = \Delta_{\rm r}G_{\rm m}^{\diamond} + RT \ln \prod_{i=1}^{k} a_i^{\nu_i}$$

Δ _r G _m	direction of a reaction	
negative	→	
zero	equilibrium	
positive	←	

Example. The equilibrium constant of reaction

 $Sn(I) + H_2O(g) \rightarrow SnO(s) + H_2(g)$

is 0.435 at T = 928 K. Mixture of H₂O + H₂ contains 65 mol.% of water vapor. Is tin oxidized or reduced? pəpnpəl \leftarrow ETZ'O = $\frac{L8}{m_D^{J}\nabla}$

Temperature dependence of *K*

⇒ (van	(υν)ρ	$\frac{H}{T^2} \Rightarrow \frac{d(\Delta_r G_{m'}^{\diamond})}{dT}$	$\frac{T}{T} = -\frac{\Delta_{\rm r} H_{\rm m}^{\oplus}}{T^2}$
		$\frac{\mathrm{d}\ln K}{\mathrm{d}T} = \frac{\Delta_{\mathrm{r}}H_{\mathrm{m}}^{\diamond}}{RT^2}$	
	∆ _r H [⊕] m	higher $T \Rightarrow K$	equilibrium shifted to
	negative (exothermic)	decreases	<
	positive (endothermic)	increases	→

Le Chatelier(-Braun) principle: Any change in status quo prompts an opposing reaction in the responding system.

If a chemical system at equilibrium experiences a change in concentration, temperature, volume, or partial pressure, the equilibrium shifts to counteract the imposed change and a new equilibrium is established.