

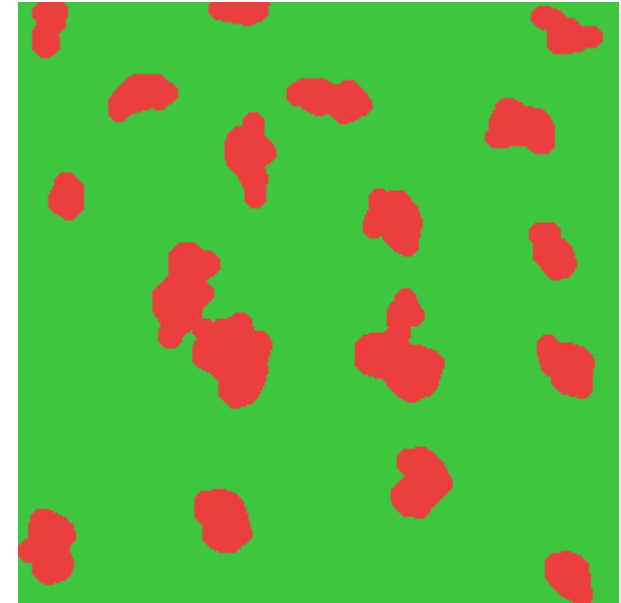
Dispersion system =  
dispersed phase in a continuum phase (medium)

s/l, l/l, ...

According to the size of the dispersed phase:

- coarse dispersion (suspension),  $> 1 \mu\text{m}$
- colloid  $1 \mu\text{m} - 1 \text{nm}$ 
  - heterogeneous (micelles, precipitates, ...)
  - homogeneous (solutions of macromolecules)
- solutions

Examples: polymer solutions, asphalt concrete, starch, milk, fresh precipitate...



- Coarse dispersions: turbidity (look as a haze), milk-like  
size  $\gg \lambda$ : white/gray (if particles are not colored)  
size  $\approx \lambda$ : Tyndall phenomenon, blue is scattered more (red Sun in dust)  
size  $\ll \lambda$ : Rayleigh scattering, blue is scattered more  
elastic scattered – photon energy does not change
- Colligative properties – measurable only in fine dispersions
- Brownian motion, diffusivity decreases as the size increases  
( $D = k_B T / 6\pi\eta R$ )
- Viscosity – bigger than the fluid medium, often non-Newton  
– plasticity = a minimum stress needed to flow, viscosity decreases with the shear strain  
– dilatancy = viscosity increases with flow speed/shear strain (starch + water)
- Density – in between both phases
- Surface tension – often lower



credit: <http://www.physics.emory.edu/~weeks/squishy/>

# Dispersion systems

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col12

Dissolved or dispersed phase	Continuous medium	Solution: Homogeneous mixture: Dissolved phase < 1 nanometer	Colloid: Dispersed phase between 1 nanometer and 1 micrometer	Coarse dispersion (Suspension): Heterogeneous mixture: Dispersed phase > 1 micrometer
Gas	Gas	Gas mixture: air (oxygen and other gases in nitrogen)	None	None
Liquid	Gas	None	Aerosol: fog, mist, vapor, hair sprays	Aerosol
Solid	Gas	None	Solid aerosol: smoke, cloud, air particulates	Solid aerosol: dust
Gas	Liquid	Solution: oxygen in water	Foam: whipped cream, shaving cream	Foam
Liquid	Liquid	Solution: alcoholic beverages	Emulsion: miniemulsion, microemulsion	Emulsion: milk, mayonnaise, hand cream
Solid	Liquid	Solution: sugar in water	Sol: pigmented ink, blood	Suspension: mud (soil, clay or silt particles are suspended in water), chalk powder suspended in water
Gas	Solid	Solution: hydrogen in metals	Solid foam: aerogel	Foam: dry sponge, styrofoam, pumice
Liquid	Solid	Solution: amalgam (mercury in gold), hexane in paraffin wax	Gel: agar, gelatin, silicagel, opal	Wet sponge
Solid	Solid	Solution: alloys, plasticizers in plastics	Solid sol: cranberry glass	Gravel, granite

Shape of particles:

- globular, isometric particles ( $r_x \approx r_y \approx r_z$ )
- lamellar, anisometric particles ( $r_x \approx r_y \gg r_z$ )
- fibrillar, anisometric particles ( $r_x \gg r_y \approx r_z$ )

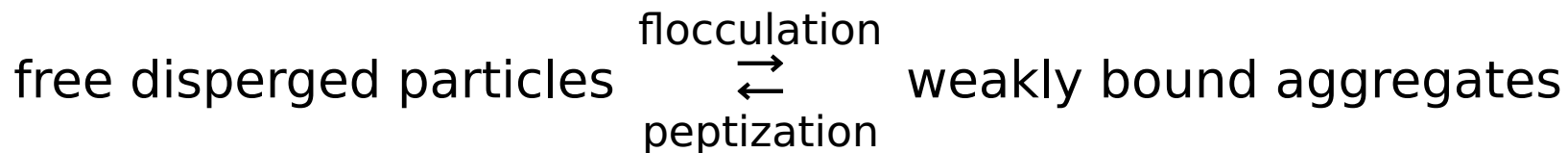
## Interactions:

- lyophilic dispersions (medium wets the particles,  $\theta < 90^\circ$ )  
in water: hydrophilic
- lyophobic dispersions (does not wet)  
in water: hydrophobic

- polymerization
- oversaturation of a solution (ouzo, anise drink)
- oversaturation of a micellar colloid (over CMC = critical micellar concentration)
- mechanically (grinding, ultrasound)
- electrically (electric arch, cathodic sputtering)
- precipitation reactions – insoluble product (AgBr in a photographic “emulsion”)

Microcrystals of a precipitate may be aggregated (flocculated), because the el. double layer is thin in a concentrated ionic solution (according to the DLVO theory), rinsing out the ions stabilizes the colloid (peptization).

Aggregation caused by weak forces:



# Distribution functions

E.g., **mass (differential) distribution function**  $F_w(m)$ :

ratio (prob = count/(total number)) of particles of masses in interval  $(m, m + dm)$  is  $F_w(m)dm$ .

Normalization:

$$\int_0^{\infty} F_w(m)dm = 1$$

Cumulative (integrated) distrib. function = ratio of particles of masses  $< m$ :

$$I_w(m) = \int_0^m F_w(m')dm', \quad Q_w(m) = \int_m^{\infty} F_w(m')dm' = 1 - I_w(m)$$

Similar: Distribution function of particle volumes, ...

- Monodisperse system – all particles of the same size (peak on  $F_w(m)$ ); may form crystals

Spheres: fcc 74%, “random close packing” 64%

- Polydisperse systems: e.g. asphalt concrete (example of random fractal)  
*try to guess the fraction of mineral filling*

Fraction = group of particles of approx. the same size (filtering, ...)

Potential of external force (e.g., gravity) =  $U$

External force:  $\vec{F} = -\text{grad } U$

asphalt concrete:  
95 % mineral filling  
5 % bitumen

**Forces of gravity** (acceleration =  $g$ ):

$$F = -mg, \quad U = mhg$$

**Forces in a centrifuge:**

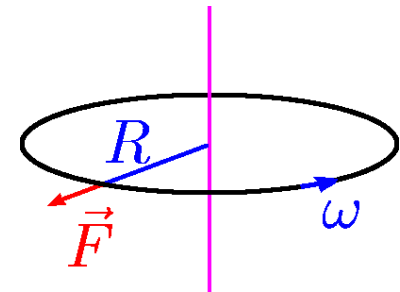
$$F = mR\omega^2, \quad U = -\frac{1}{2}m(R\omega)^2, \quad \omega = 2\pi\nu = \frac{2\pi}{\tau}$$

$\omega$  = angular (circular) frequency

$\nu$  = frequency (in Hz or RPM, 1 RPM =  $\frac{1}{60}$  Hz)

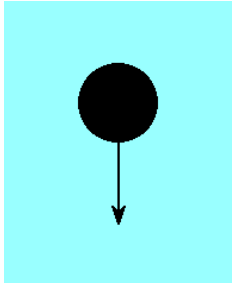
$R$  = radius of rotation

$\tau$  = period



# Speed of sedimentation

- Density of particles =  $\rho_1$
- Density of dispersion medium =  $\rho$
- Viscosity of dispersion =  $\eta$
- Particle volume =  $V_1$
- Friction coefficient =  $f$
- Sedimentation speed =  $v$



## In the field of gravity:

The force must be corrected for the buoyant force (Archimedes' principle):

$$F = V_1(\rho_1 - \rho)g, \quad v = \frac{F}{f} = \frac{V_1(\rho_1 - \rho)g}{f}$$

Spherical particles:  $V_1 = \frac{4}{3}\pi r^3$ ,  $f = 6\pi\eta r$  (Stokes)

$$v = \frac{2r^2}{9\eta}(\rho_1 - \rho)g$$

**In a centrifuge:** use  $R\omega^2$  instead of  $g$

(typical 1000g – 10,000g, ultracentrifuge up to  $10^6g$ )

Small particles sediment slowly. Molecules sediment, too (very slowly): uranium enrichment by centrifugation of  $UF_6(g)$



## From Boltzmann probability

Ideal solution: concentration  $\propto$  Boltzmann probability  $\Rightarrow$

$$c(\vec{r}) = c_0 \exp\left(\frac{-U(\vec{r})}{k_B T}\right)$$

In a gravitational field this is the barometric formula:

$$c(h) = c(0) \exp\left(\frac{-V_1(\rho_1 - \rho)gh}{k_B T}\right)$$

In a centrifuge of angular frequency  $\omega = 2\pi \times$  frequency:

$$c(r) = c(0) \exp\left(\frac{\frac{1}{2}V_1(\rho_1 - \rho)(R\omega)^2}{k_B T}\right)$$

where  $\Delta m = V_1(\rho_1 - \rho)$

## From the speeds of sedimentation and diffusion

$$v_{\text{sedimentation}} = \frac{F}{f} = -\frac{\nabla U}{f}$$

$$v_{\text{diffusion}} = \frac{J}{c} = -\frac{D\nabla c}{c} = -D\nabla \ln c = -\frac{k_B T}{f} \nabla \ln c$$

$$v_{\text{sedimentation}} + v_{\text{diffusion}} = 0 \Rightarrow c = c_0 \exp\left(-\frac{U}{k_B T}\right)$$

Let  $\mu$  be per particle (not mole), infinite dilution approximation:

$$\mu = \mu_0 + k_B T \ln(c/c^{\text{st}}) \Rightarrow v_{\text{diffusion}} = -\frac{1}{f} \nabla \mu$$

Thus

$$v_{\text{sedimentation}} + v_{\text{diffusion}} = 0$$

is equivalent to

$$U + \mu = \text{const}$$

Some time ago, we used the **assumption** of  $U + \mu = \text{const}$  to **derive**  $D = k_B T / f$

## Examples

**Example.** The equilibrium concentration of monodisperse oil droplets in a cuvette 10 cm tall is twice as large near the surface than at the bottom. Calculate the diameter of oil droplets. The temperature is 25 °C, the density of water is  $0.997 \text{ g cm}^{-3}$ , the density of oil is  $0.920 \text{ g cm}^{-3}$ .

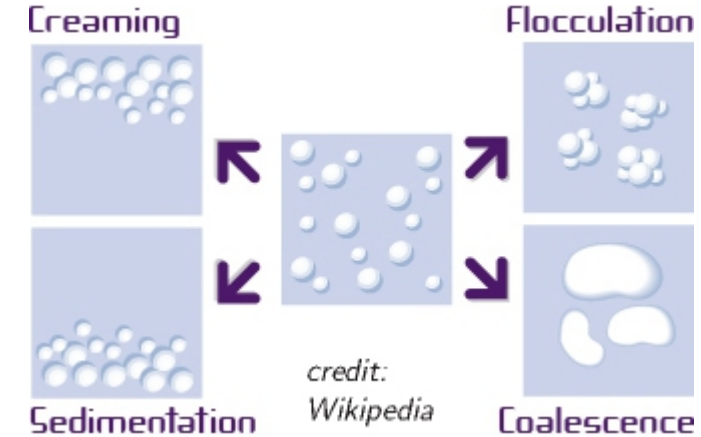
42 nm

**Example.** Consider a globular protein of molecular weight of 20 kDa. What is the speed of sedimentation in a centrifuge of 24000 RPM at a point 5 cm from the axis? The density of the protein is  $1.35 \text{ g cm}^{-3}$ , the viscosity of water is  $0.891 \text{ mPa s}$ .

$$V_1 = 2.46 \times 10^{-26} \text{ m}^3, r = 1.8 \text{ nm}, \nu = 0.32 \text{ mm h}^{-1}, a = 32200g$$

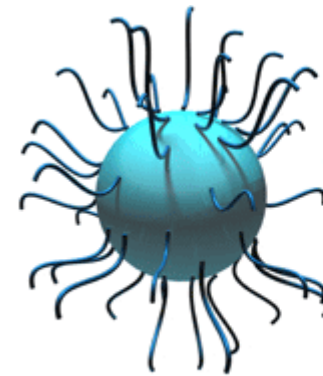
Dispersions are thermodynamically metastable (large interface)

- sedimentation ( $\downarrow$ ), creaming ( $\uparrow$ )
- flocculation (reversible), coagulation (irreversible)
- coalescence (of droplets)
- Ostwald ripening (small  $\rightarrow$  large, Kelvin equation)

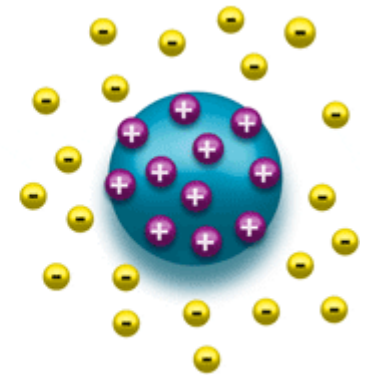


## Stabilization:

- by electric double layer  
DLVO theory (see below)
- steric (adsorption of macromolecules in a good solvent)
- depletion (macromolecules in between particles)
- electrosteric
- kinetic (in a very viscous medium)

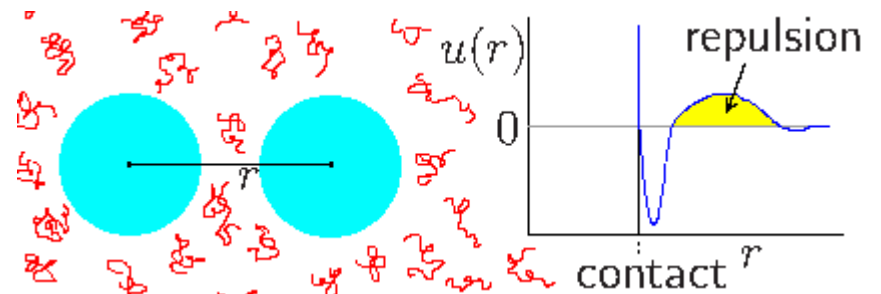


Steric stabilization



Electrostatic stabilization

credit: <http://www.malvern.jp/>



Deryagin (Дерягин, Derjaguin) + Landau (Ландау),  
Verwey + Overbeek.

- repulsion of charged surfaces (screened by a Gouy–Chapman (diffusion) layer) stabilizes a colloid
- attractive dispersion (London) forces tries to stick particles together

Stability is a result of a competition between both forces

- surface charge increases stability
- dispersion forces decrease stability

Diffusion (Gouy–Chapman) layer, 1:1 electrolyte, small  $\phi e/k_B T$ :

$$\phi = \phi_0 e^{-x/\lambda}, \quad \text{where } \lambda = \sqrt{\frac{\epsilon R T}{2 c F^2}}$$

Surface charge = – layer charge

$$\sigma = - \int_0^{\infty} (\rho_+ - \rho_-) dx = - \int_0^{\infty} c F \left\{ \exp \left[ -\frac{\phi(x) e}{k_B T} \right] - \exp \left[ \frac{\phi(x) e}{k_B T} \right] \right\} dx$$

$$\text{For small } \frac{\phi(x) e}{k_B T}: \quad \sigma \approx \int_0^{\infty} 2 c F \frac{\phi(x) e}{k_B T} dx = 2 \lambda c F \phi_0 \frac{e}{k_B T} = \frac{\epsilon}{\lambda} \phi_0$$

$\epsilon/\lambda$  = capacity of the Gouy–Chapman double layer (per unit area)

Energy (per unit area) of the surface charge  $\sigma$  in potential  $\phi_0$  is (in the superposition approximation, that's why multiplied by 2)

$$E_{\text{elst}} = 2 \sigma \phi_0 e^{-d/\lambda} = 2 \frac{\lambda \sigma^2}{\epsilon} e^{-d/\lambda} = 2 \frac{\epsilon \phi_0^2}{\lambda} e^{-d/\lambda}$$

Formulas for curved interfaces are more complex, however, the leading term is always  $e^{-d/\lambda}$

For 2 molecules  $r$  apart ( $r \gg$  overlap of orbitals), the energy decays as  $\propto 1/r^6$ :

$$u(r) = -\frac{C}{r^6}$$

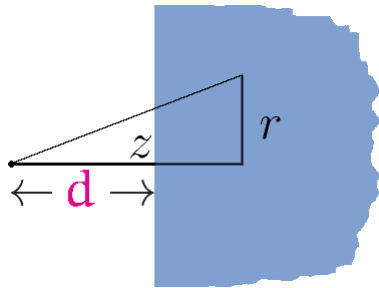
- charge–charge:  $u \propto 1/r$
- dipole–charge:  $u \propto 1/r^2$  (fixed dipole orientation)
- dipole–dipole:  $u \propto 1/r^3$
- Freely rotating dipole–freely rotating dipole:  $u \propto 1/r^6$
- Dipole–induced dipole:  $u \propto 1/r^6$
- London (dispersion) force (fluctuating dipole–fluctuation dipole):  
fluctuation  $\Rightarrow$  dipole  $\Rightarrow$  el. field  $\propto 1/r^3 \Rightarrow$  induced dipole  $\propto 1/r^3 \Rightarrow u \propto 1/r^6$   
Usually the most pronounced
- London force for  $r \gg 1\mu\text{m}$ :  $u \propto 1/r^7$ .

$$u(r) = -\frac{C}{r^6}$$

Contributions from atom pairs are considered as independent (valid to  $\sim 80\text{--}90\%$ )

For two bodies we make a sum (integral); e.g., for a slit:

Point-surface (half-space) first:

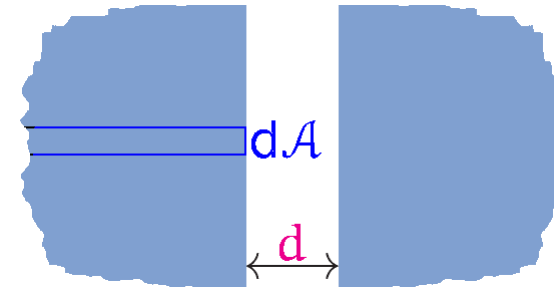


$$u_{\text{wall}}(d) = -\mathcal{N}C \frac{2\pi}{12d^3}$$

$\mathcal{N} = N_A n / V =$  number density

$A = (\pi\mathcal{N})^2 C =$  **Hamaker constant** of given substance,  $[A] = \text{J}$

Then a column of area  $dA$ :



$$E_{\text{vdW}} = -\frac{\pi\mathcal{N}^2 C}{12d^2} = -\frac{A}{12\pi d^2}$$

(per unit area)

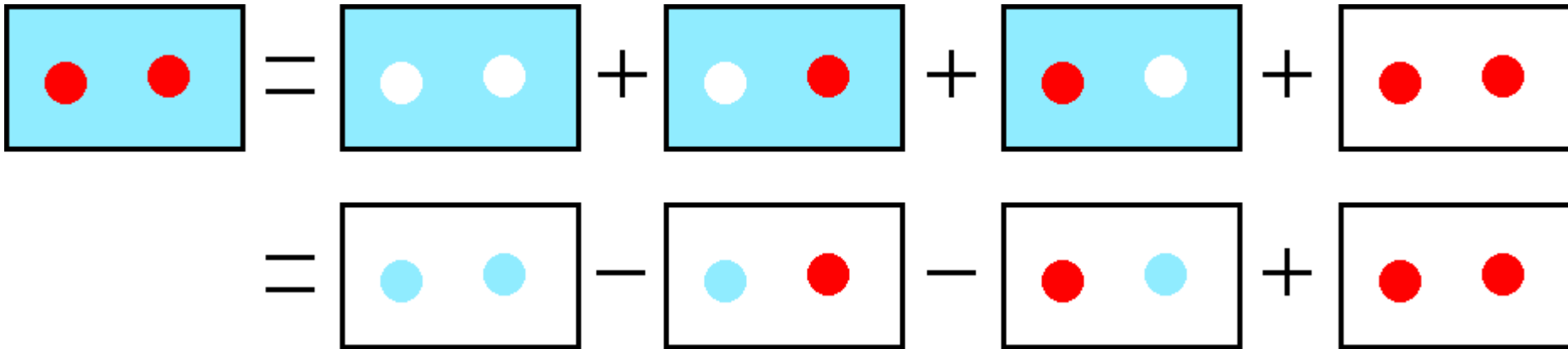
Two  $R$ -balls  $d$  apart, first term of the expansion in  $d \ll R$ :  $E_{\text{vdW}} = -\frac{AR}{12\pi d}$



Cross interaction between both media,

$$u_{12}(r) = -\frac{C_{12}}{r^6}, \quad A_{12} = \pi^2 \mathcal{N}_1 \mathcal{N}_2 C_{12}$$

Particles of **2** in material **1** (0 = particles far away)



$$A_{1/2} = A_{11} - 2A_{12} + A_{22}$$

Approximation (combining rule):

$$A_{12} \approx \sqrt{A_{11}A_{22}}$$

Then

$$A_{1/2} = \left( \sqrt{A_{11}} - \sqrt{A_{22}} \right)^2$$

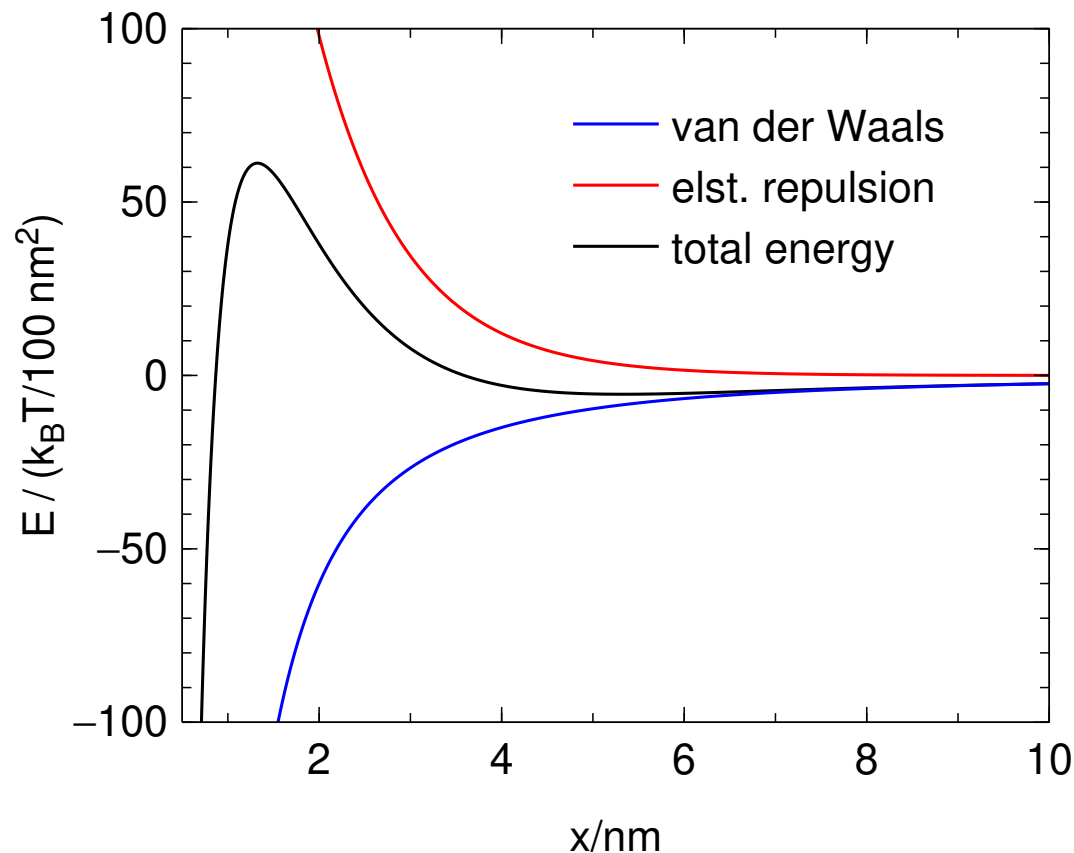
# DLVO: case study

TiO<sub>2</sub> in a  $\odot$  of NaCl.

$$A(\text{TiO}_2) = 19.5 \times 10^{-20} \text{ J}, A(\text{H}_2\text{O}) = 3.7 \times 10^{-20} \text{ J}, \Rightarrow A \approx 6.2 \times 10^{-20} \text{ J}$$

- flat interface formulas
- energy expressed in  $k_B T$  per 100 nm<sup>2</sup>
- figure:  $\phi_0 = 0.15 \text{ V}$ ,  $c = 0.1 \text{ mol dm}^{-3}$

$k_B T$  = thermal “quantum”



barrier  $60 k_B T / 100 \text{ nm}^2$

$$e^{-E/k_B T} = e^{-60} = 1 \times 10^{-26}$$

↓

cubes of side 10 nm will be stable

Rule of the thumb:  
stable for barrier  $> 25 k_B T$

$$e^{-25} \approx 10^{-11}$$

- Diffusivity of a spherical particle of diameter  $2R = 10$  nm (Stokes formula):

$$D_i = \frac{k_B T}{6\pi\eta R_i} = \frac{1.38 \times 10^{-23} \text{ J K}^{-1} \times 298 \text{ K}}{6\pi \times 0.89 \times 10^{-3} \text{ m}^{-1} \text{ kg s}^{-1} \times 5 \times 10^{-9} \text{ m}} = 5 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$$

- If the particles are about  $r = R$  apart, the typical collision time is

$$\tau \approx \frac{r^2}{6D} = \frac{(5 \times 10^{-9} \text{ m})^2}{6 \times 5 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}} = 1 \times 10^{-7} \text{ s}$$

- For the probability of barrier crossing of  $\pi = e^{-25} = 10^{-11}$ , the typical timescale of flocculation is:

$$\frac{\tau}{\pi} \approx 10000 \text{ s} \approx \text{hours}$$

- surfaces close together (at contact): attraction (adhesion)
- surfaces far away: fast decreasing attraction
- medium distances (according to the potential): energy barrier

The barrier grows = stability increases for:

- potential (surface charge) increases (in abs. value)
- salt concentration decreases (longer Debye screening range)