

# Granulace

## Granulation

*F. Štěpánek & J. Lindner, 2011-13*

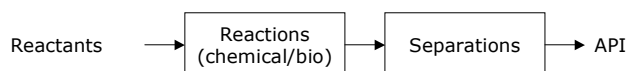


Evropský sociální fond  
Praha & EU: Investujeme do vaší budoucnosti

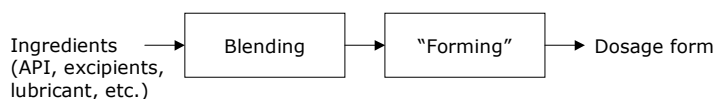
### Pharmaceutical Process Development

- 1) API manufacturing - "primary" processing
  - Reaction route selection
  - Solids isolation (crystallisation, filtration, drying)
- 2) Dosage form manufacturing - "secondary" processing
  - Types of dosage forms
  - Processing routes

#### Primary:



#### Secondary:



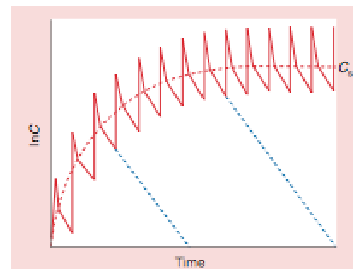
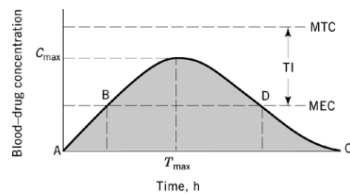
## Dosage form design

### Administration routes:

- **oral** (tablets, capsules, liquids)
- **pulmonary** (aerosols, inhalation powders)
- **transdermal** (creams, controlled-release adhesive patches)
- **intra-venous** (e.g. vaccines, insulin, antibiotics)
- **"direct application"** (e.g. eye drops, skin cream)
- **implantable controlled-release devices**

### Pharmacokinetic considerations:

- Bioavailability
- Required dose (drug "potency")
- Instant release vs. delayed/controlled release
- One off vs. chronic administration



## 1. Absorption

## 2. Distribution

## 3. Elimination

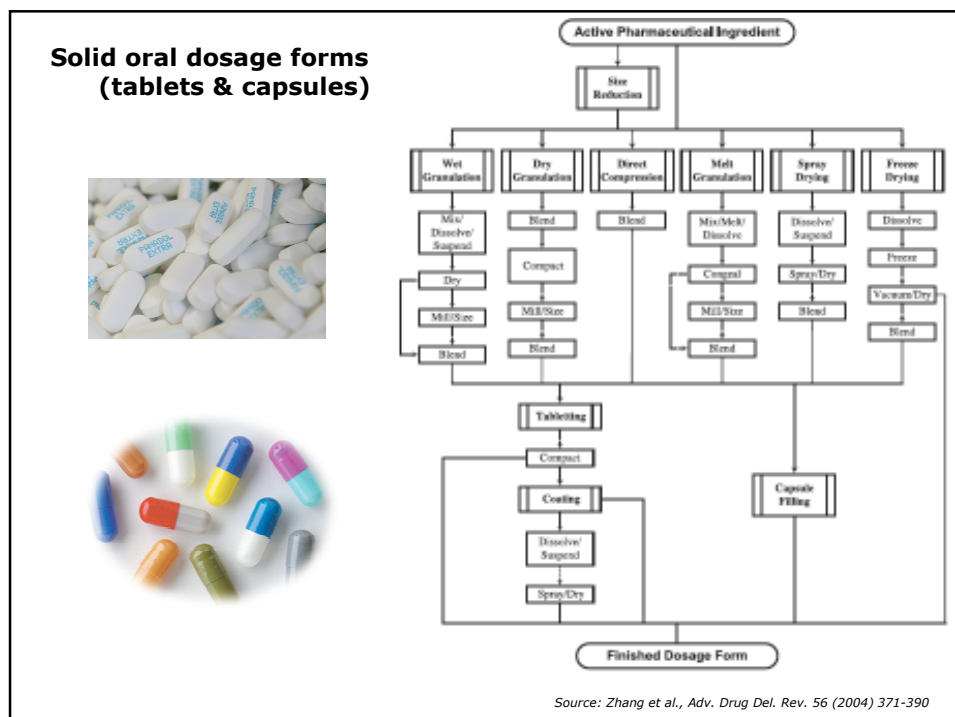
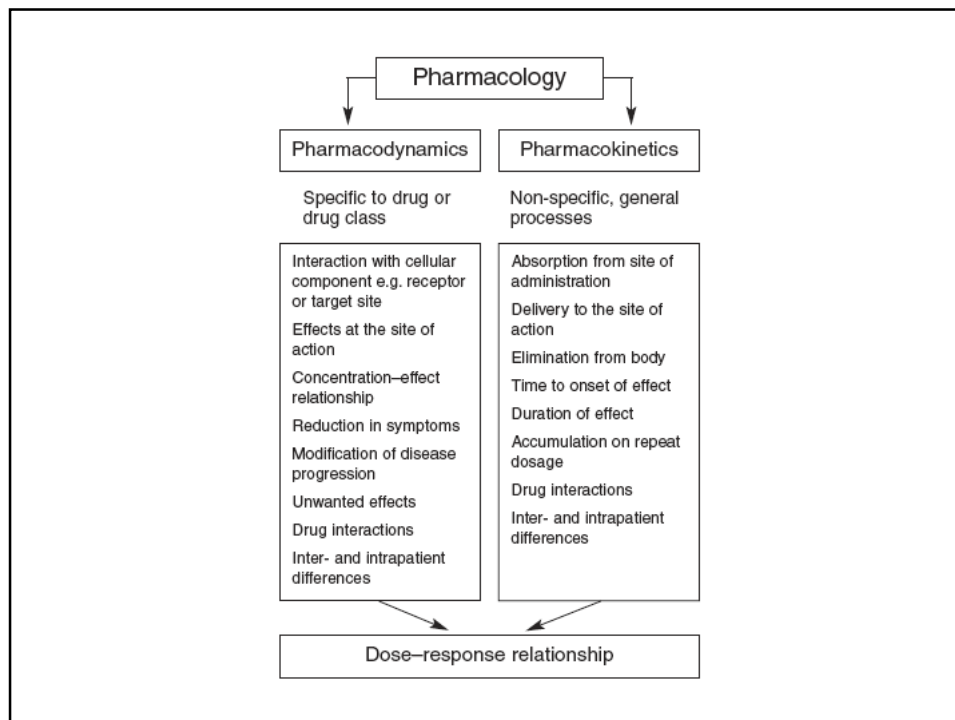
### 3.a Metabolism

### 3.b Excretion

**Bioavailability  $F$**  = the fraction of the administered dose that reaches the systemic circulation as the parent drug (not as metabolites)

### **Apparent volume of distribution**

$V$  = Total amount of drug in the body / Plasma concentration



## Powder Blending

Measure of mixedness - variance of composition

$$\sigma^2 = \sum (w_i - w_{avg})^2 / n \quad (n \dots \text{number of samples, } w_i \dots \text{mass fraction})$$

Mixing number  $N_{mix}$  - number of unit mixing operations required for the system to reach a given state of mixedness

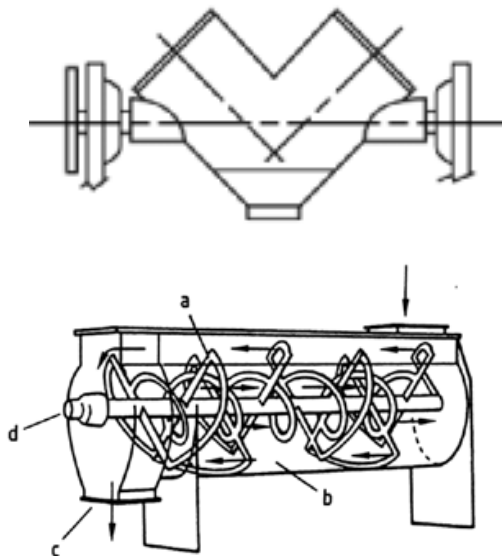
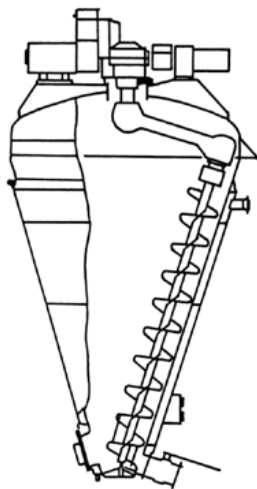
Segregation - natural tendency of powders to de-mix due to difference in particle size, shape, density or surface properties (friction, cohesion)

- occurs during transport (conveying) or storage (IBCs) of powders
- need to "freeze" a well-mixed state immediately after blending

Mixing equipment

- both batch and continuous
- mechanical agitation
- commonly used: V-blender

## Powder blending equipment



## Wet Granulation

Principle: contact powder with a liquid binder, wet powder particles become cohesive, agglomeration occurs during particle collisions, binder sets to form mechanically stable granules.

Binder types:

- melt binders ~ melts, solidify upon cooling (e.g. PEG)
- aqueous binders ~ solutions, solidify upon drying (e.g. HPC, PVP)
- water ~ partial dissolution and recrystallisation of ingredient(s)

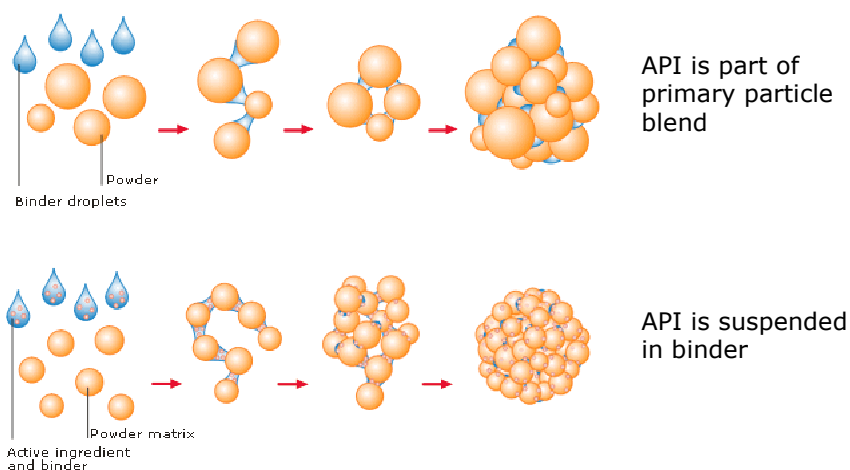
Binder application:

- spray (liquid atomisation) for low-shear processes
- mechanical dispersion in high-shear processes

Granulation processes:

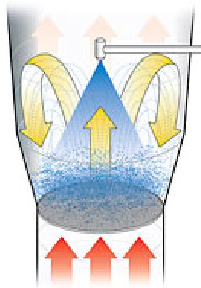
- fluid bed granulation
- high-shear mixer granulation

## Wet granulation



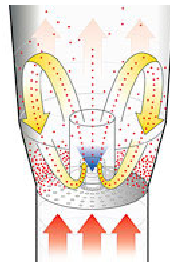
## Fluid bed granulation

Top spray

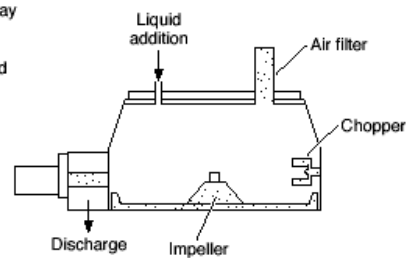
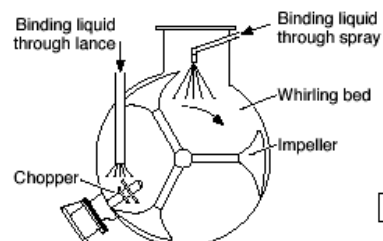


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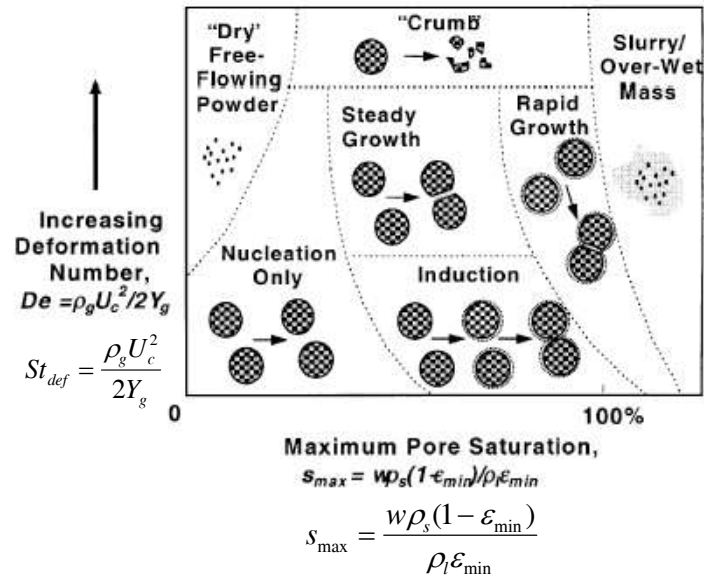
Bottom spray  
(Wurster coater)



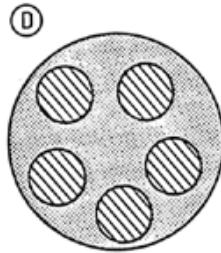
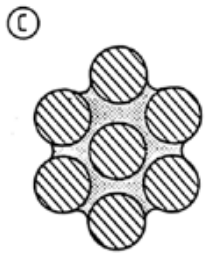
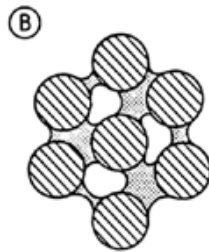
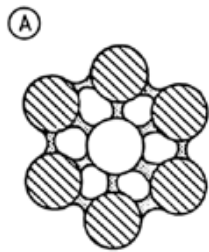
## Batch high-shear mixer-granulator



**Growth regime map** (Iveson & Litster, *AIChE J* **44**, 1510, 1998)



Liquid distribution in a wet granule:



- A) pendular
- B) funicular
- C) capillary
- D) droplet

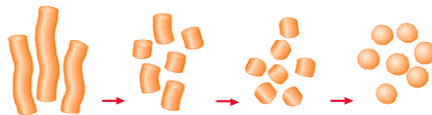
## Extrusion-spheronisation

### Principle of operation:

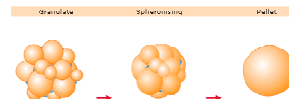
- Prepare a paste from API, excipients, binder, water
- Extrude paste through screen to form "noodles"
- Contact extrudates with a high-speed rotating disk
- Dry resulting spherical pellets



Extruded product    Breaking up    Spheronising    Pellets



...but it is also possible to carry out spheronisation after wet granulation



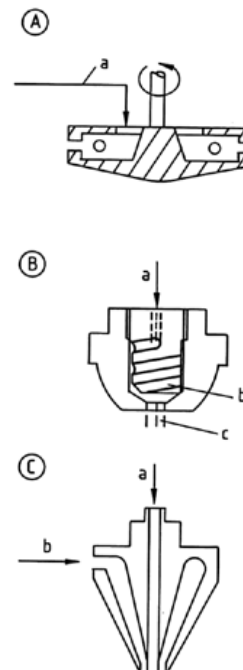
## Spray drying

Step 1: solution or slurry preparation  
= dissolution/suspension of primary solid particles in a liquid

Step 2: liquid atomisation = formation of droplets of the slurry  
nozzle types:

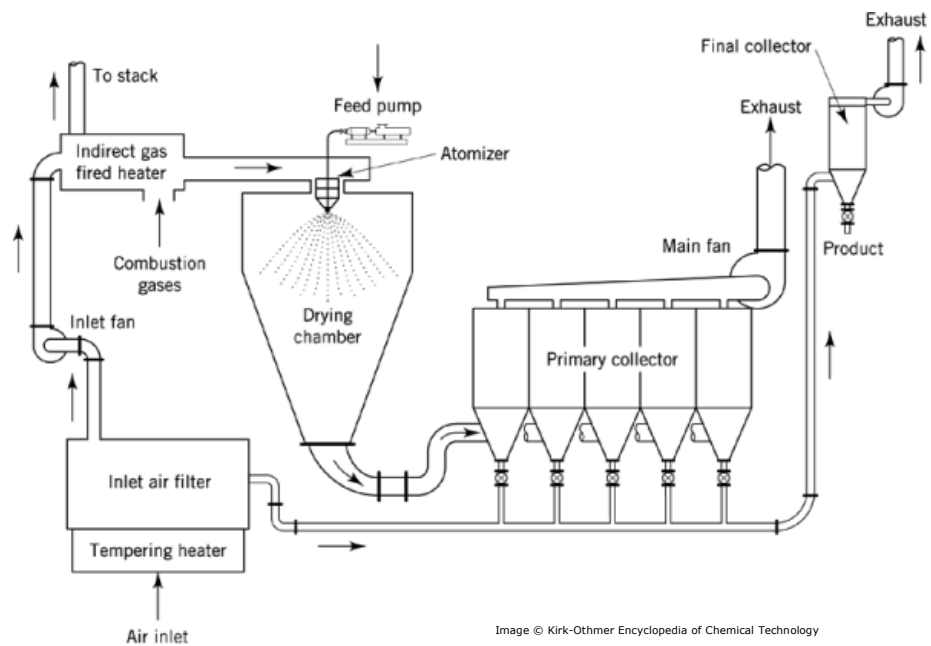
- rotary nozzle
- single phase pressure nozzle
- two phase nozzle

Step 3: particle formation =  
evaporation of liquid from the droplets  
leaves behind a (porous) solid structure





### Spray drying - process set-up



### Spray drying - process equipment

Pilot plant scale



### Calculation of drying time

Evaporation rate:  $m' = Q / \Delta h_v$

Heat-transfer rate:  $Q = h_q A \Delta T$

Heat-transfer coefficient from gas to a single droplet:

$$Nu = 2.0 + 0.60 Re_p^{1/2} Pr^{1/3}$$

$$(Nu = h_q d / \lambda \quad Re = u d \rho_g / \mu \quad Pr = c_{pg} \mu / \lambda)$$

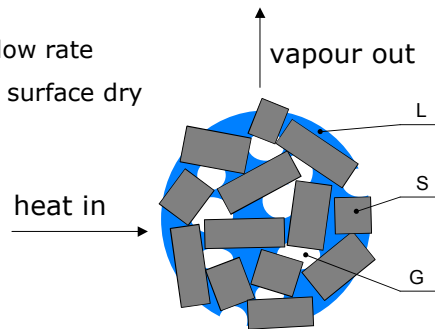
$u$  ... relative air velocity

Fast initial rate of drying => Skin formation

Energy balance: Gas temperature and flow rate

Residence time need to be sufficient for surface dry particles to be formed

Often followed by fluid bed drying

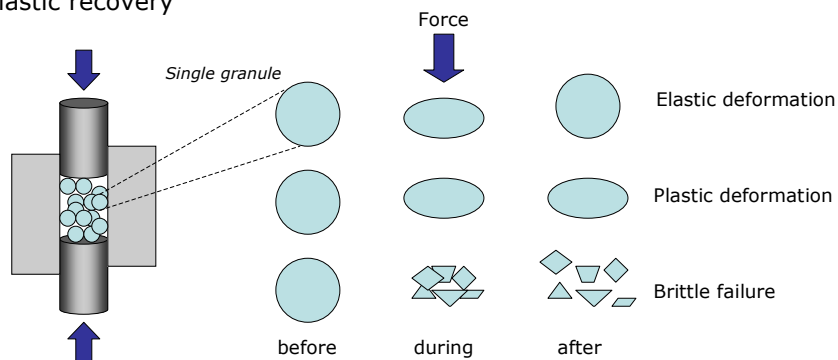
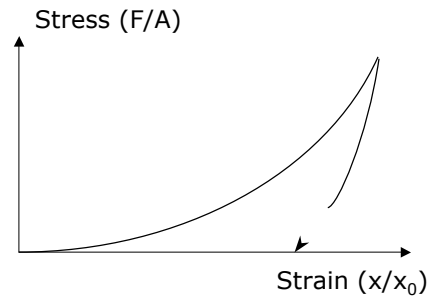


### Tabletting

#### Powder compressibility

Phenomena:

- Rearrangement
- Elastic deformation
- Plastic deformation and/or viscous flow
- Brittle failure
- Elastic recovery



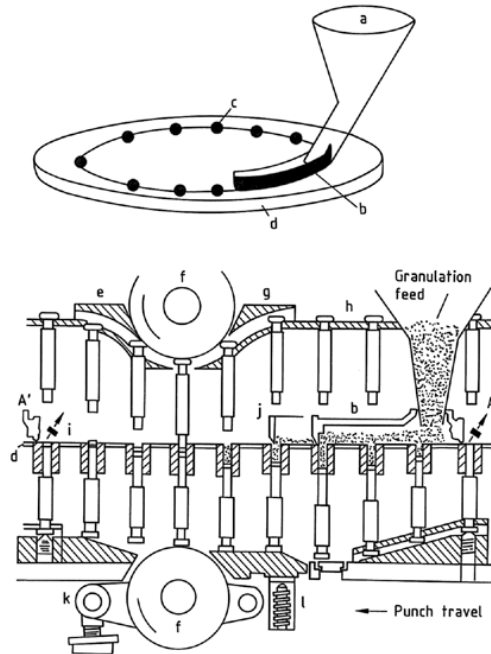
## Tablet compaction

Cyclic operation:

- Feed
- Pre-compact
- De-aerate
- Final compaction
- Eject

Need to use lubricants (e.g. magnesium stearate) to avoid sticking to punch or die walls and reduce wear.

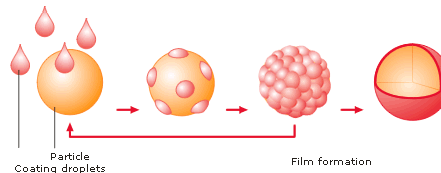
Problems:  
capping, de-lamination



## Coating

Aims of coating:

- Taste masking
- Visual appeal (coloured tablets)
- Protective layer (abrasion)
- Delayed release effect (gastric fluid resistance)
- Functional coating of carrier particles - API



Typical film thickness 5-50  $\mu\text{m}$

Coating rate determined by:

- Bed turnover rate
- Drying rate

Criteria for coating vs. agglomeration:

$$St_v = \frac{8\tilde{m}u_0}{3\pi\mu\tilde{D}^2} \leq St_v^* = 2\ln\left(\frac{\lambda}{h_a}\right)$$

$St_v$  : viscous Stokes

$\tilde{m}$  : number

$\tilde{D}$  : reduced particle mass

$u_0$  : reduced particle

diameter

$u_0$  : velocity of collision

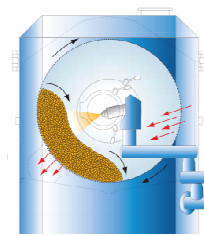
$\mu$  : binder viscosity

$\lambda$  : thickness of

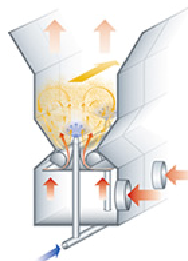
binder layer

$h_a$  : particle surface

roughness



1. Drum coater



2. Spouted bed  
3. Wurster coater  
(see earlier)

## Plant layout

Vertical flow principle:

- processing stations on different levels
- gravity flow

Horizontal flow principle:

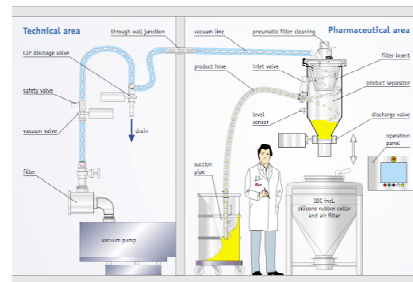
- processing stations on the same floor
- transport by IBC's or pneumatic conveying system

## Solids handling

IBC = Intermediate Bulk Container



## Pneumatic conveying



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