

Sušení

Drying

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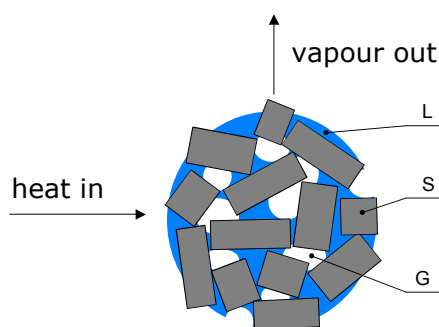


Evropský sociální fond
Praha & EU: Investujeme do vaší budoucnosti

Drying

Filtration/Centrifugation - mechanical separation of liquid from solids

Drying - separation by L-V phase transition



Composition - solid material:

A ... liquid; B ... solid

dry basis:

$$x_A = m_A / m_B$$

wet basis:

$$w_A = m_A / (m_A + m_B)$$

Composition - gas phase:

partial pressure

$$p_A = y_A P$$

relative saturation

$$\varphi = p_A / p_A^*$$

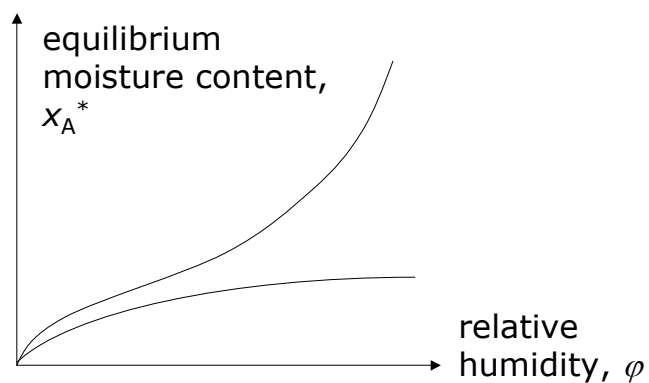
saturated vapour pressure

$$p_A^* = p_A^*(T)$$

(e.g. from Antoine equation)

Moisture equilibrium:

- free moisture content $x_A = x_{A,\text{tot}} - x_A^*$



Classification of drying processes

Means of heat supply:

- direct heat transfer (hot gas)
- indirect heat transfer (heat exchange surface, microwave, or radiative)

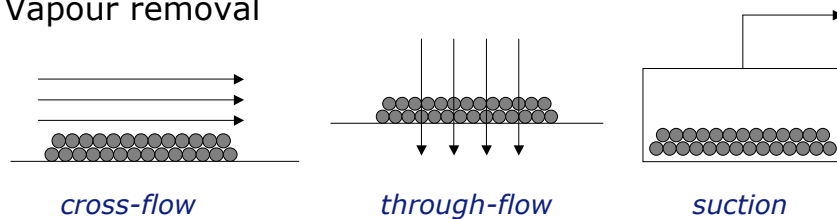
Means of vapour removal:

- cross-flow of carrier gas
- through-flow of carrier gas
- suction

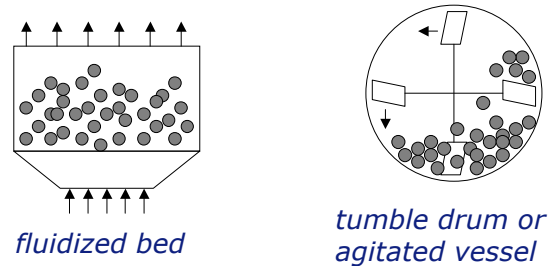
Means of solids motion:

- static vs. agitated (mechanically, fluidisation)

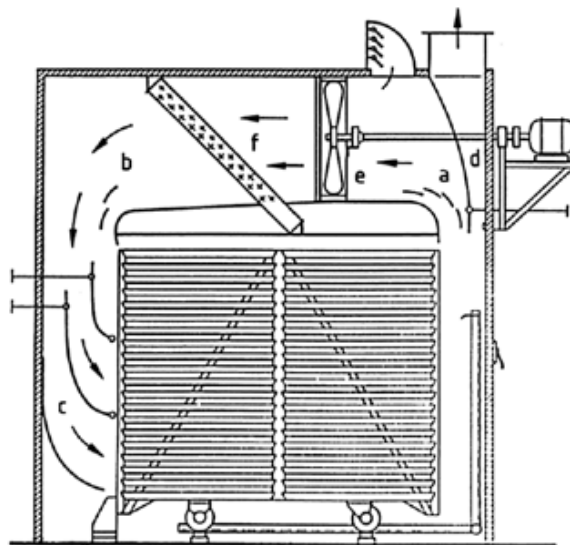
Vapour removal



Solid phase motion

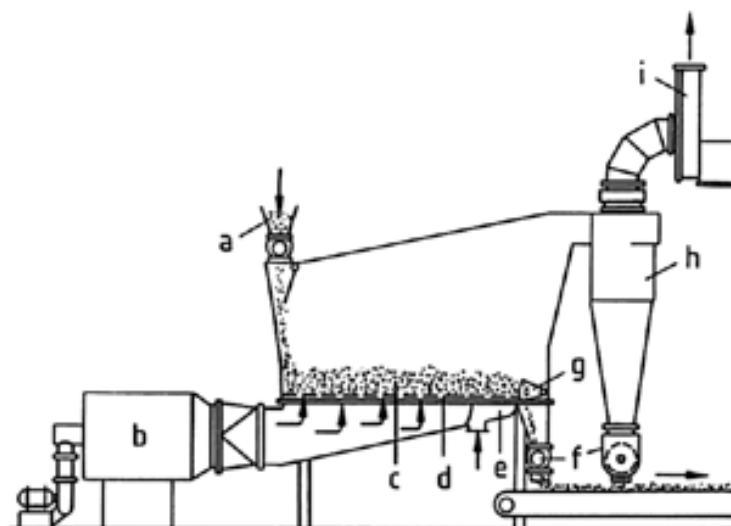


Drying equipment: tray dryer



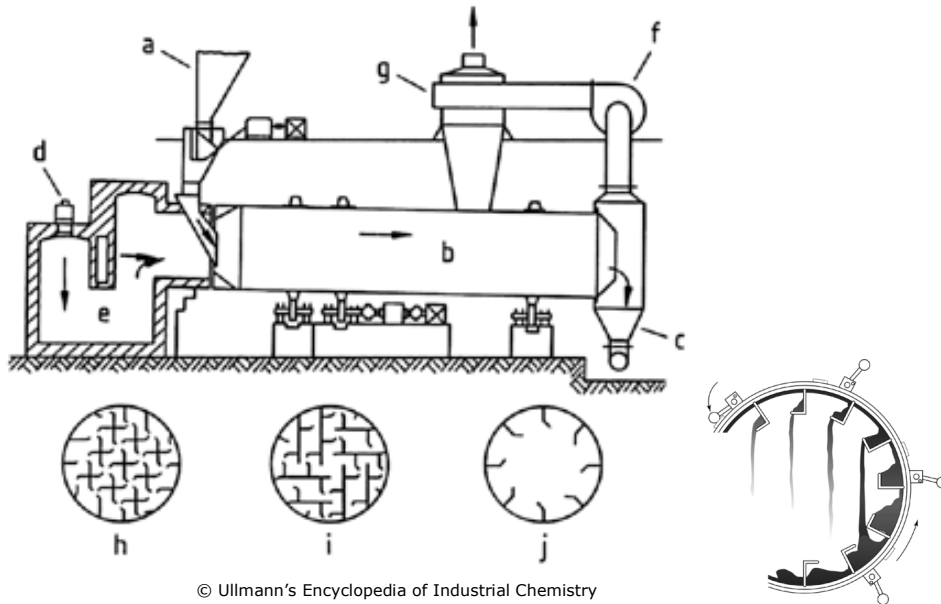
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Drying equipment: fluid-bed dryer

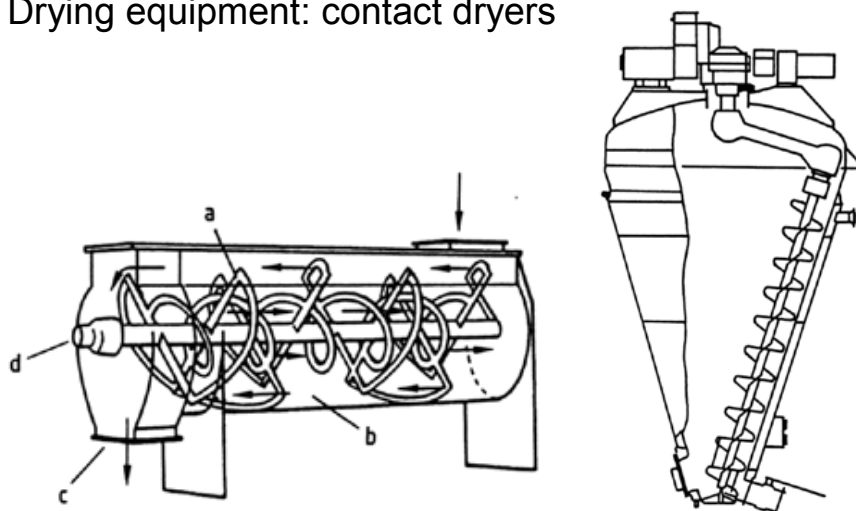


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Drying equipment: rotary drum dryer



Drying equipment: contact dryers



Horizontal agitated vessel

Cone mixer

Heat-transfer rate:

$$Q = h_q A \Delta T \quad \text{or} \quad Q = h_q aV \Delta T$$

ΔT ... mean temperature difference, $\Delta T \sim (T_h - T_v)$

(not necessarily ΔT_{LM})

Heat-transfer coefficients:

-from gas to a single particle (or droplet)

$$Nu = 2.0 + 0.60 Re_p^{1/2} Pr^{1/3}$$

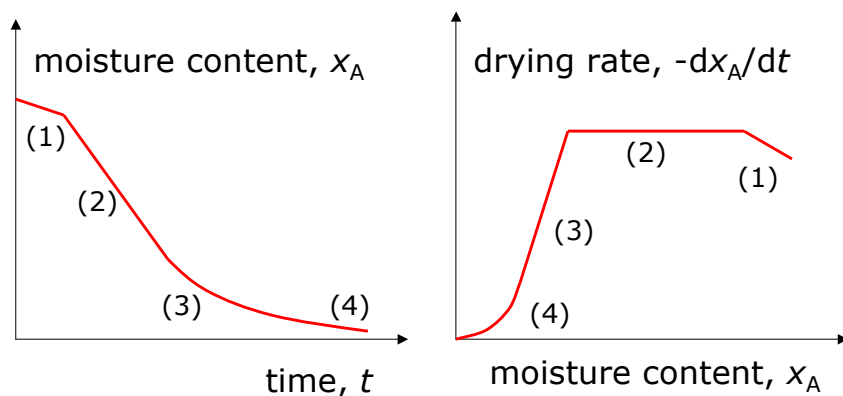
-from fluid to a flat surface (laminar flow and $Pr > 0.7$)

$$Nu = 0.664 Re^{1/2} Pr^{1/3}$$

$$(Nu = h_q L / \lambda \quad Re = uL\rho/\mu \quad Pr = c_p\mu/\lambda)$$

-otherwise correlations for each geometric arrangement

Drying curves and drying rates:



1) warming-up period

2) constant-rate period

3) 1st falling-rate period

4) 2nd falling-rate period

Calculation of drying time:

-Constant drying conditions

$$\text{Drying rate } R = - (1/A) dm_A/dt = - (m_B/A) dx_A/dt$$

$$\text{Drying time } t_T = (m_B/A) \int_{x_1}^{x_2} dx_A/R$$

$$\text{Constant period: } R = R_c \Rightarrow t_c = m_B (x_1 - x_2) / (AR_c)$$

$$\text{Falling rate period: } R = a x_A + b \quad a = (R_c - R')/(x_c - x')$$

$$\Rightarrow t_f = m_B / (aA) \ln(R_1/R_2)$$

If single falling-rate period and $x'_c=0$, then total time:

$$t_T = m_B / (AR_c) [(x_{\text{initial}} - x_c) + x_c \ln(x_c/x_{\text{final}})]$$